



UNIVERSITY of MARYLAND
SCHOOL OF PHARMACY

Developing the Control Strategy for Pharmaceutical Manufacturing Across Scales of Manufacturing

CERSI Meeting 2013

Control Strategies for Pharmaceutical Manufacturing: Real Time Release Testing and Design

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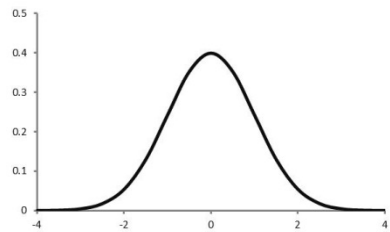


Outline

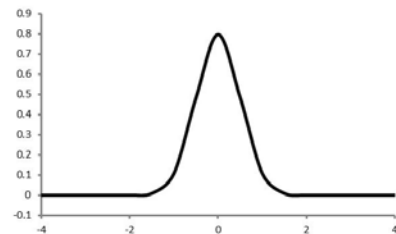
- Introduction
- Case study: Fluid bed coating of multiparticulate beads
 - Process efficiency
 - Extent of curing
 - Loss on drying
 - Dissolution & data fusion
- Summary

Note, in the interest of time, only selective steps will be shown for each model

Dosage Form Variability

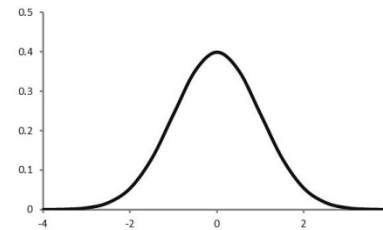


Excipients

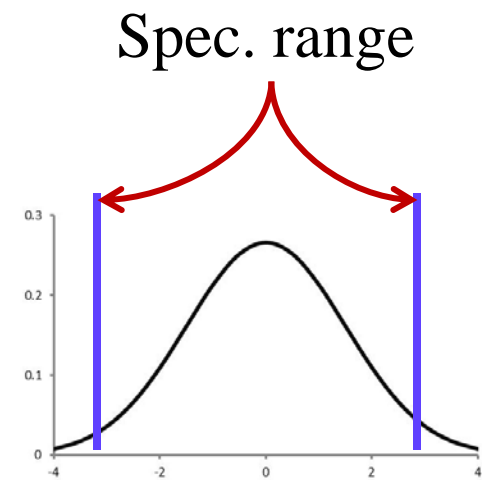


API

Processing
Conditions



Dosage
Form



$$\sigma_{Tot} = \sigma_{Exc} + \sigma_{API} + \sigma_{PC} + \sigma_{Int} + \sigma_{Mes}$$

Implementing a Control Strategy

- **Definitions - ICH Q10**
- **“Control Strategy is a **planned** set of **controls**, derived from current **product and process understanding** that **assures** process performance and product **quality**”**
- **Includes parameters and attributes of:**
 - **Drug substance**
Drug product materials and components
 - **Facilities**
 - **Equipment operating conditions**
 - **In-process controls**
 - **Measurement types and frequency of monitoring**
 - **Finished product specifications and testing**

Developing a Control Strategy

- **Essence of developing a control strategy**
 - 1) **Process understanding: ID all likely sources of variability that affects product quality**
 - 3) **Using QTPP & design space to determine acceptance ranges**
 - 2) **Develop a plan to monitor these variables**
 - **Sensor Selection – soft sensors**
 - **Chemometric model development**
 - 4) **Data usage**
 - **Oh “gosh” we have a problem**
 - **Ideally use monitoring data to feed-forward and or feedback into process**
 - **Area that needs more development**
- **If done well → Real Time Release Testing RTRT**

Prediction & Identification of Patterns

- **In data rich environment key question:**
 - Which variables & samples do you use to a build model
- **Minimalist strategy**
 - Use a narrow range of variables and samples
 - Use only variables → highly correlated to attribute
 - Use only samples → in sweet spot of design space
 - i.e., only variation in model is directly correlated with parameter of interest
 - Very good for accurate and precise prediction
- **Maximalist strategy**
 - Use all/most variables
 - Samples spanning the knowledge space with good & bad batches
 - i.e., lots of variation for many different sources
 - Very rugged, but not as accurate or precise
 - For some events predictions can be difficult
 - eg., it may be hard to predict release parameter like dissolution

Variable Selection - Example

Key Message

- To fully implement RTRT system, you need to a **comprehensive** approach
 - For example the validity of a model may depend:
 - Upon the nature of the starting materials
 - Processing conditions
 - Thus need to ensure these conditions are met
- Can use a **combination** of different model types
 - **RTRT model** may use minimalist approach
 - **MV process control chart** use maximalist approach
- Core GMP concept is to have a comprehensive plan to control all likely critical process inputs
 - When have a sufficient process control models should be predictive and rugged
- Note: may begin implementation 1 step at a time



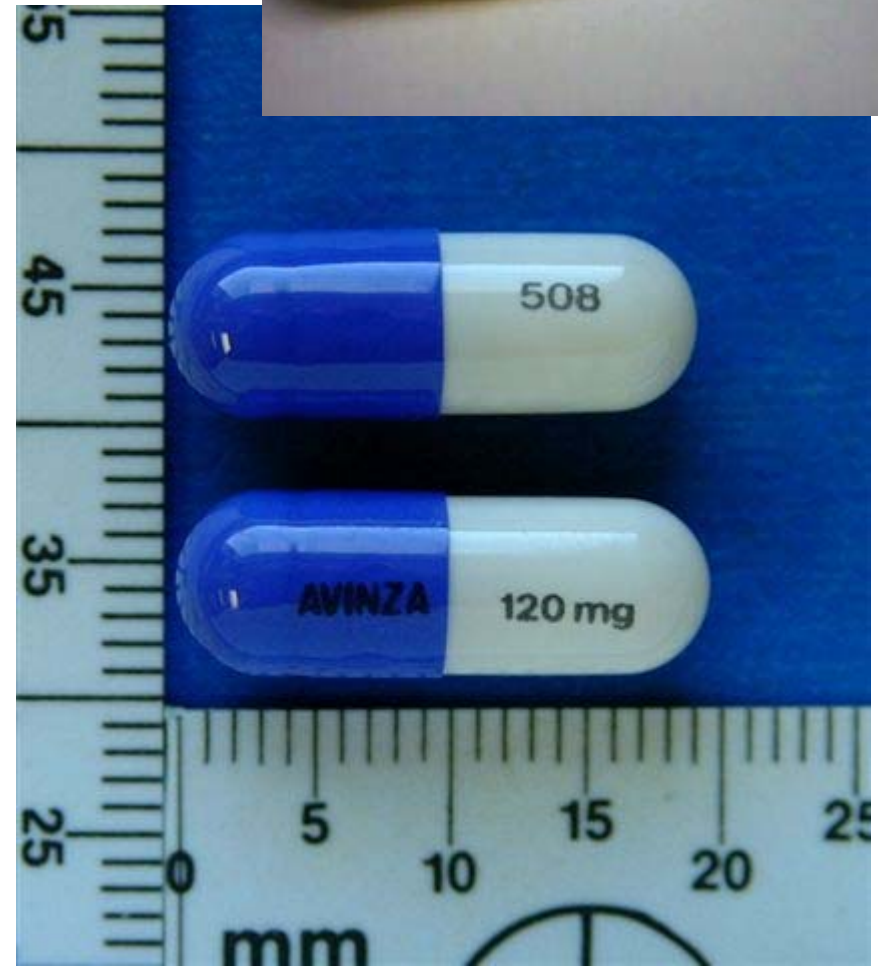
Outline

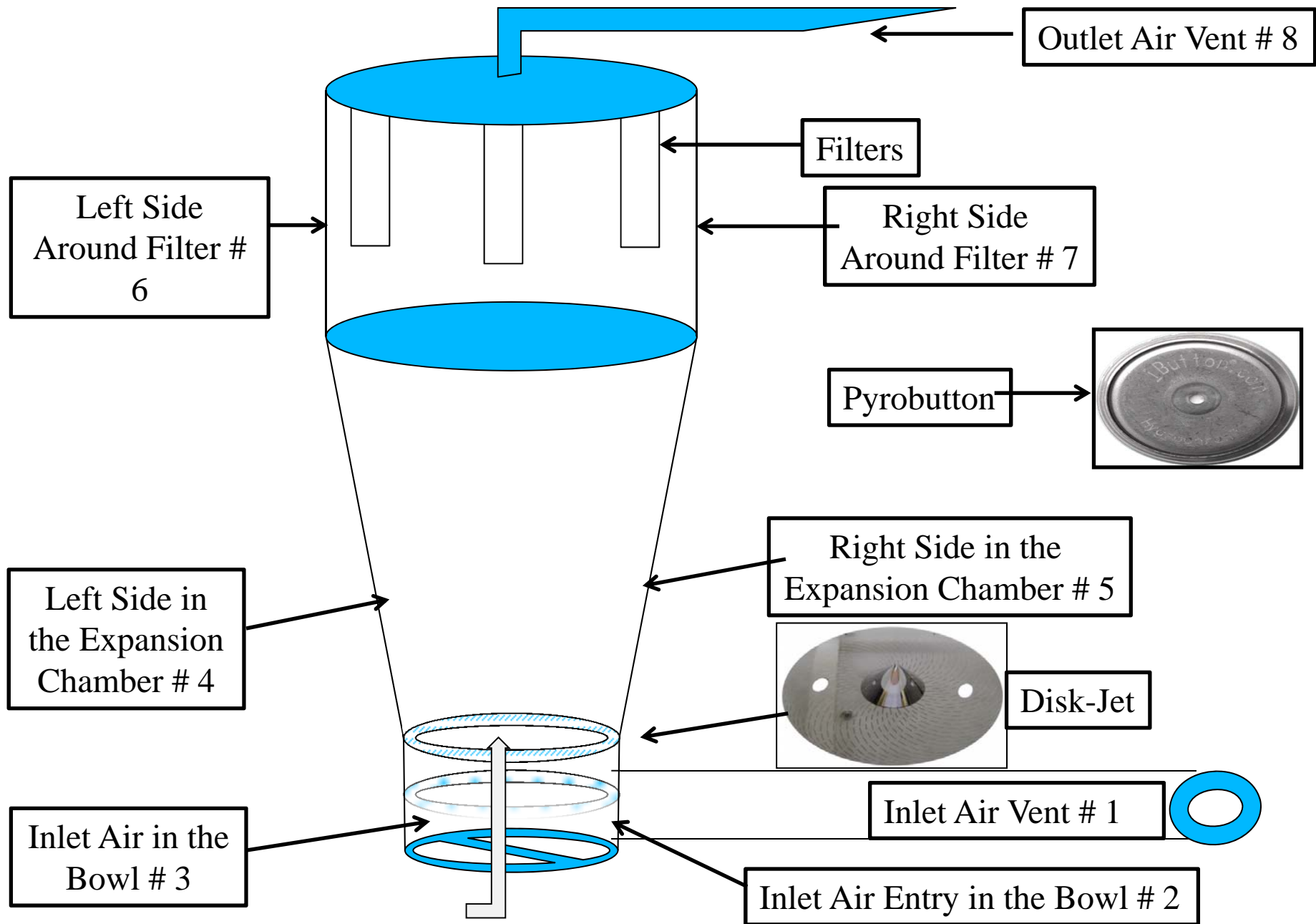
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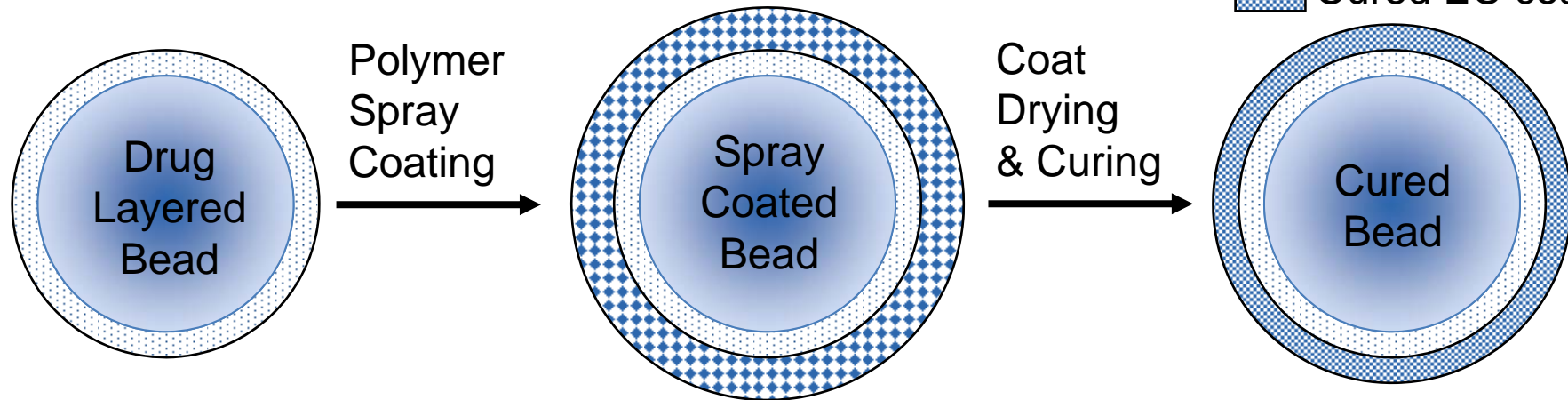
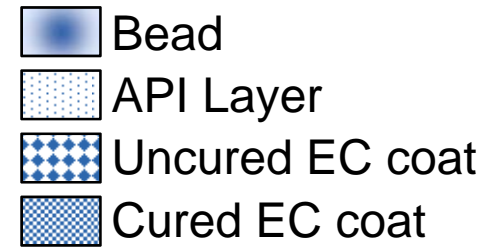
Multiparticulate Dosage Form

- e.g., Avinza
- Morphine sulfate pentahydrate
- Successful multiparticulate dosage form
- Combines IR with CR for once day dosing



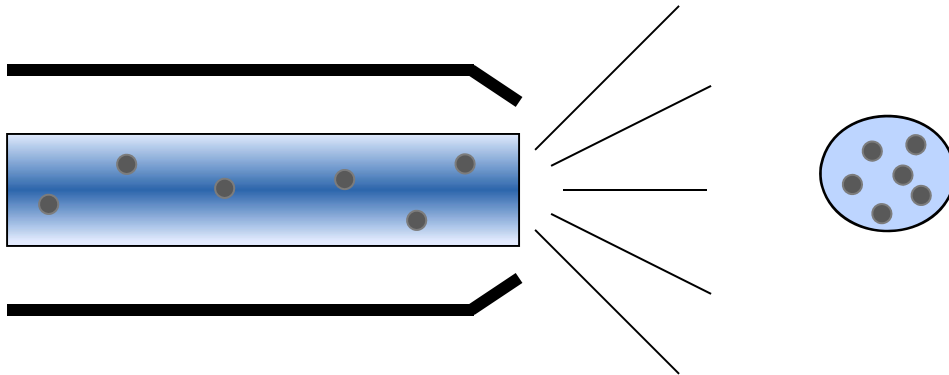


Spray Coating Beads



| | | | | | |
|--|---------------------------|---|--|--|-------------------------|
| <ul style="list-style-type: none"> - API Content - API Homogeneity - Particle Size | | CMA/CQA | | <ul style="list-style-type: none"> - Water content - Extent of curing | |
| | | <ul style="list-style-type: none"> - Thickness - Uniformity | | | |
| <ul style="list-style-type: none"> - <i>Atomization</i> - <i>Spray rate</i> - Air flow - Air temp. | | CPP | | <ul style="list-style-type: none"> - Air flow - Air temp - Curing time - LOD | |
| API assay | Process Efficiency | Models | | Moisture Content Curing Time | Dissolution Rate |

Process Efficiency

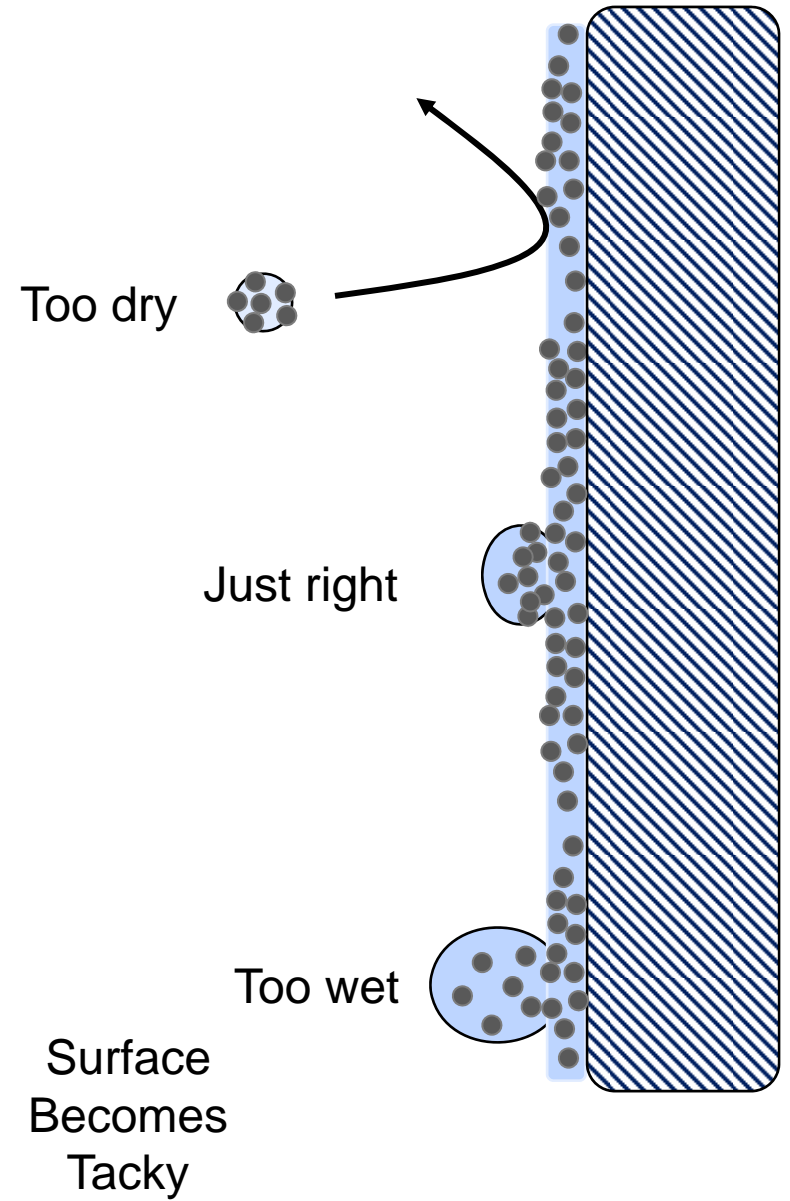


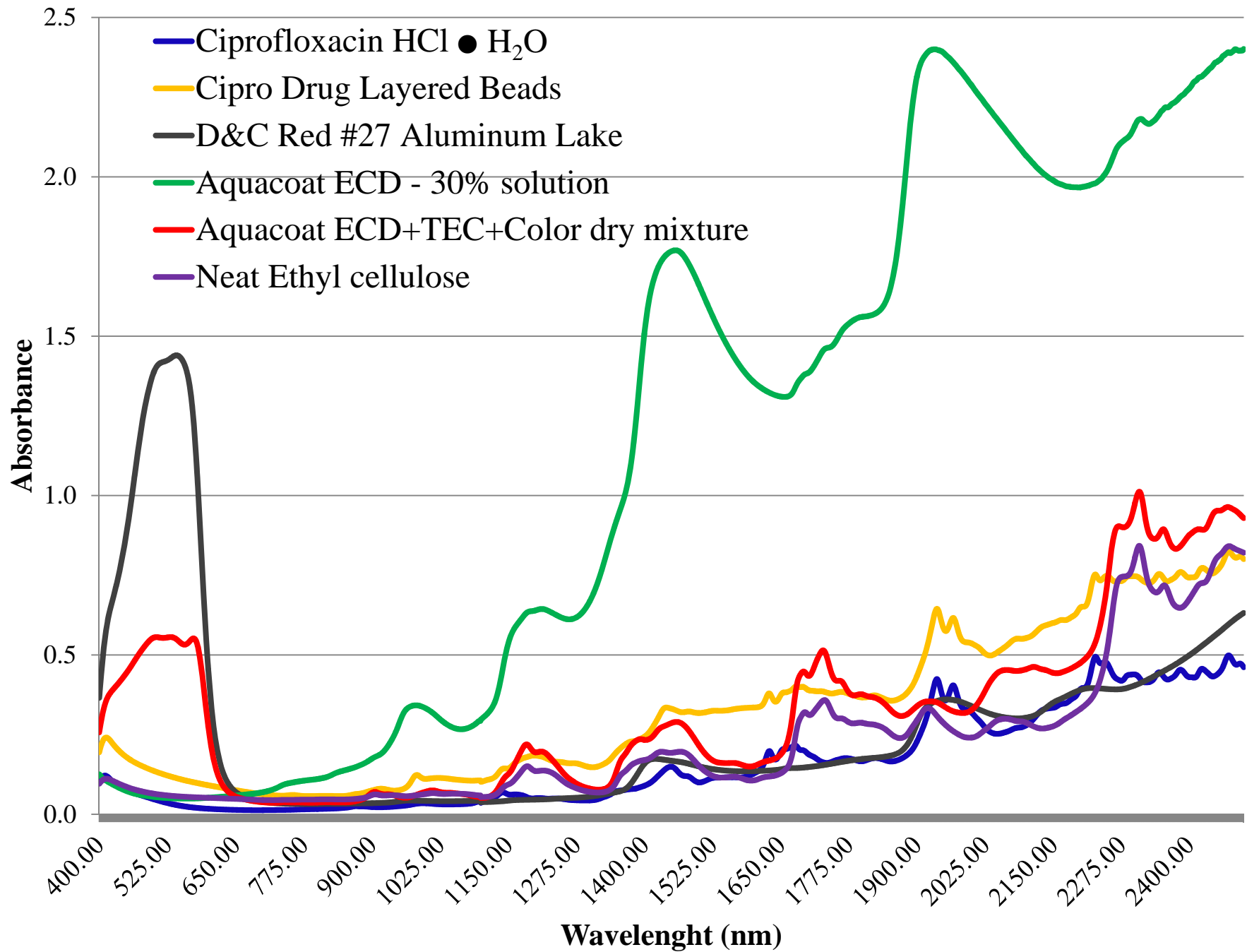
Rate of diffusion Fick's Law

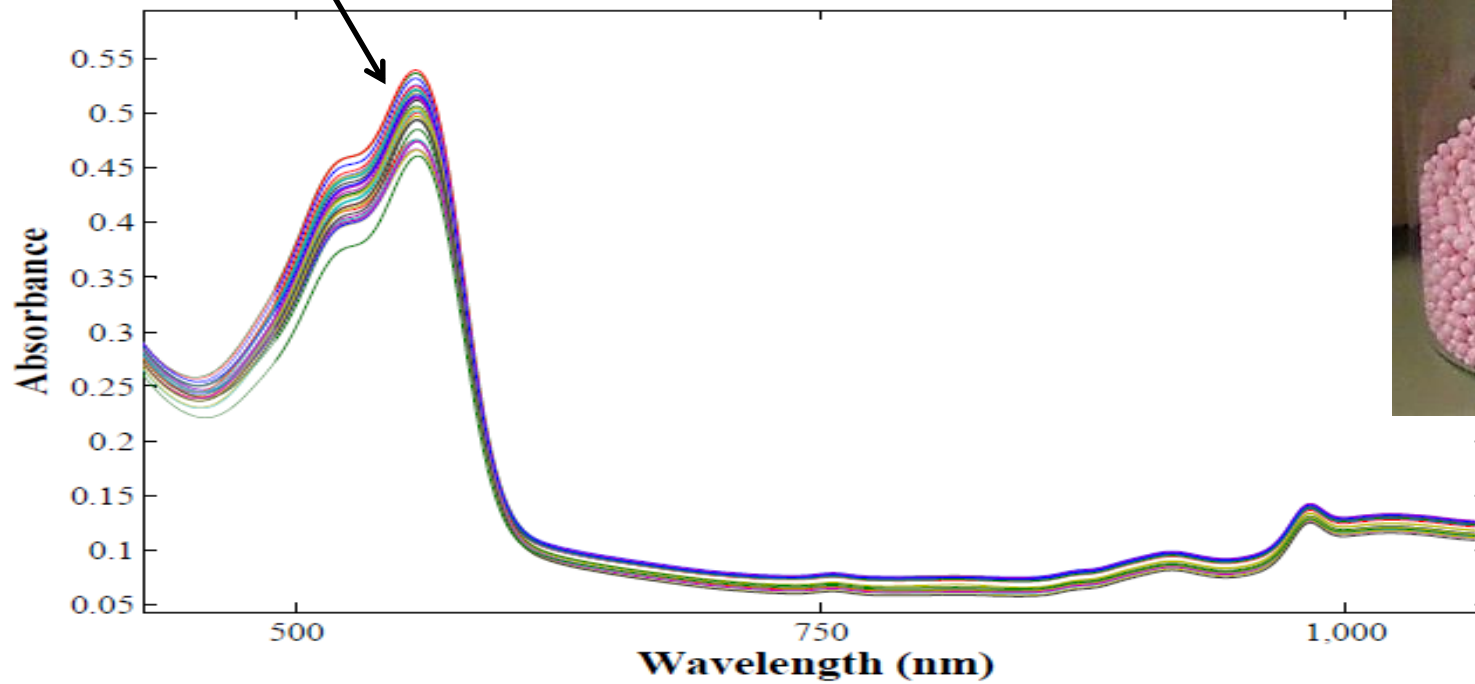
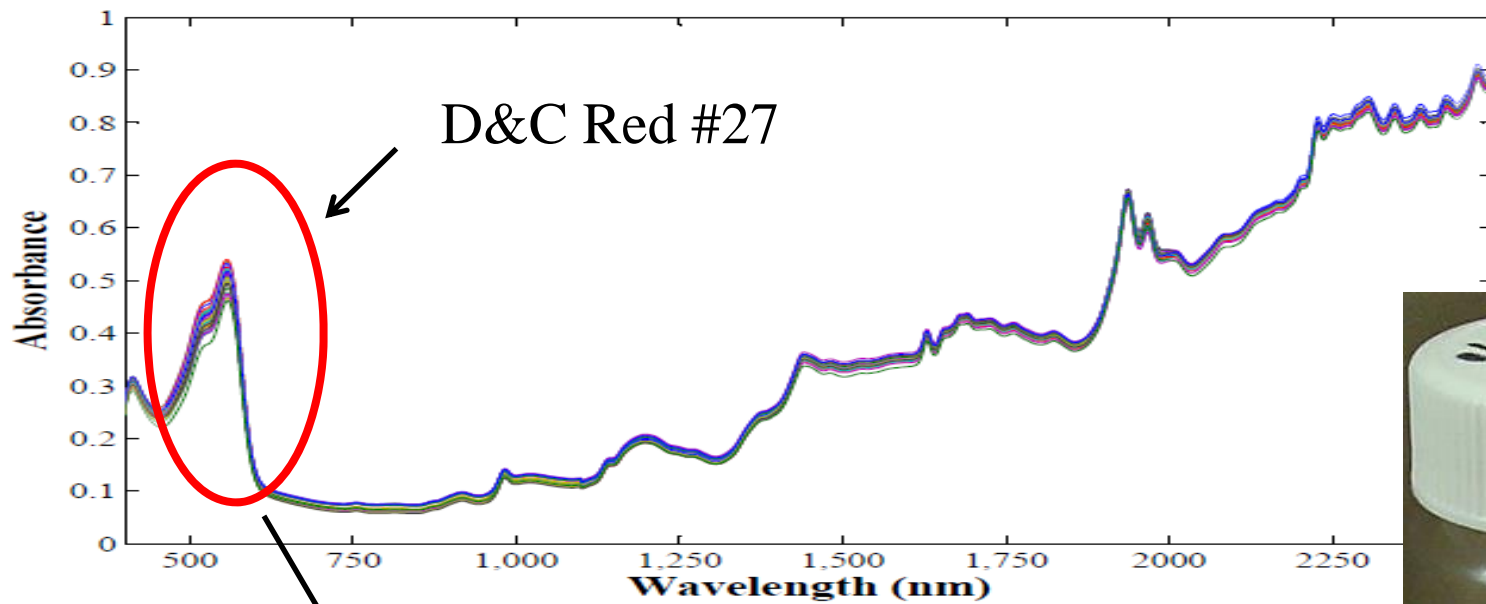
$$\frac{dm}{dt} = \frac{SD}{h} (C_{in} - C_{out})$$

h

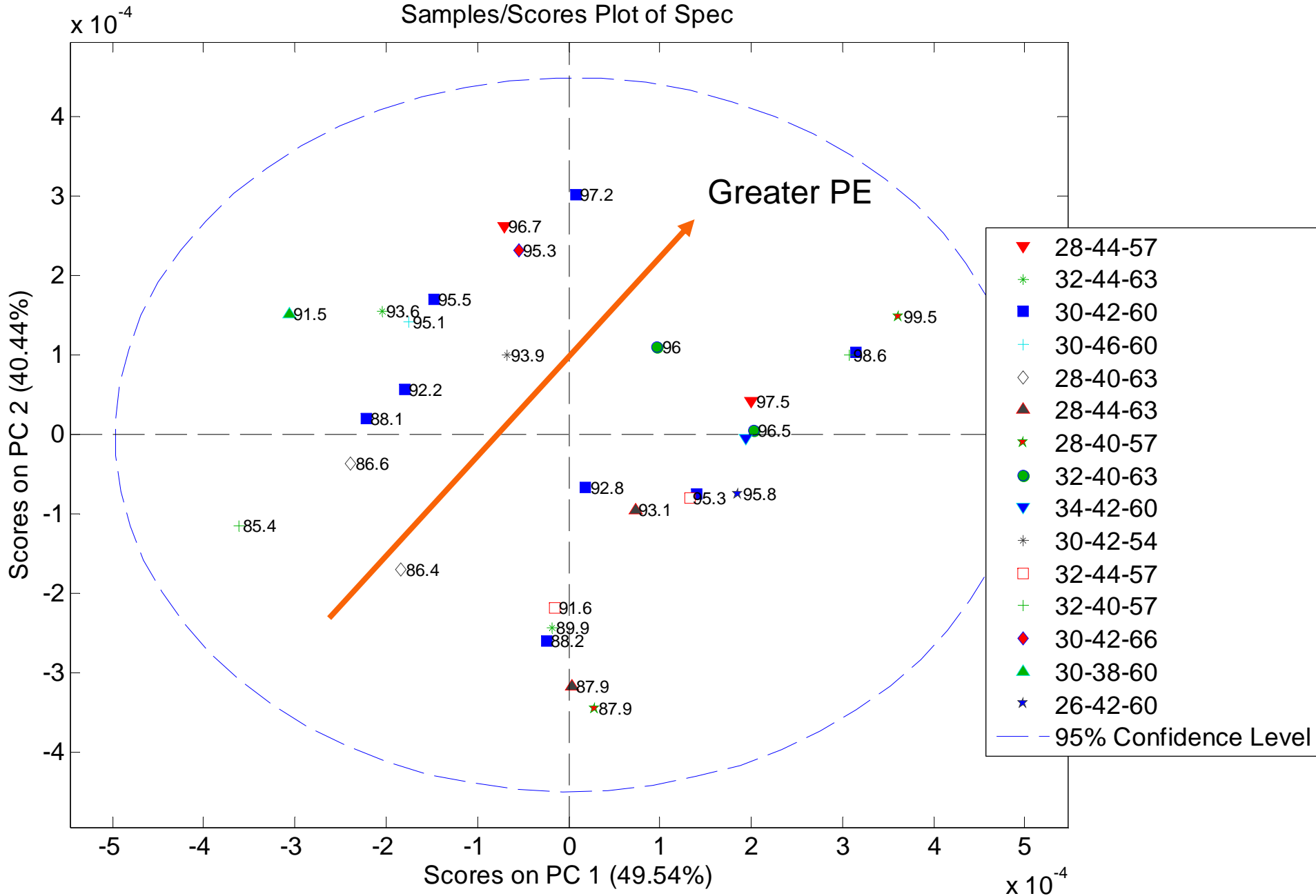
Process Efficiency





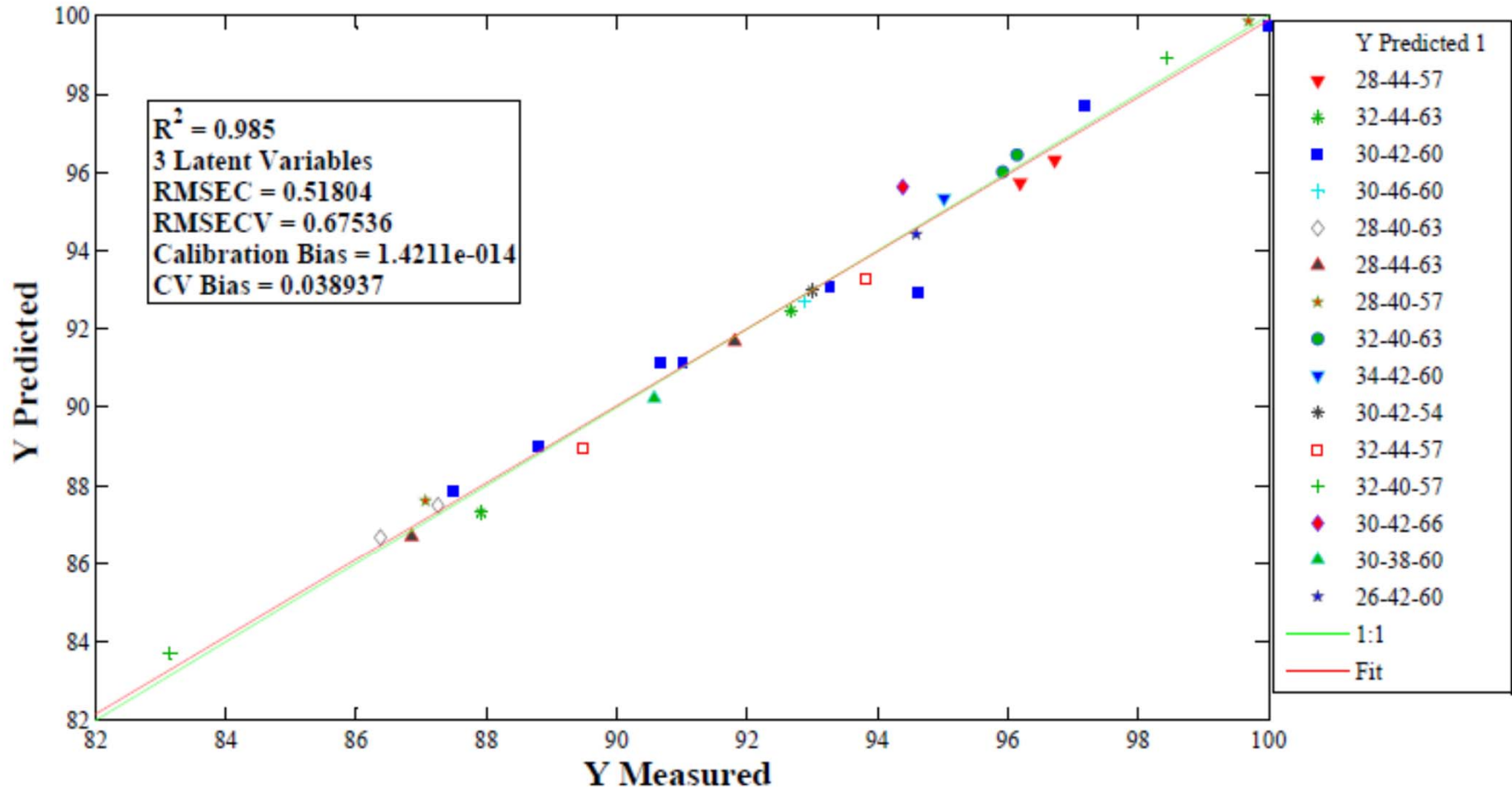


Samples/Scores Plot of Spec

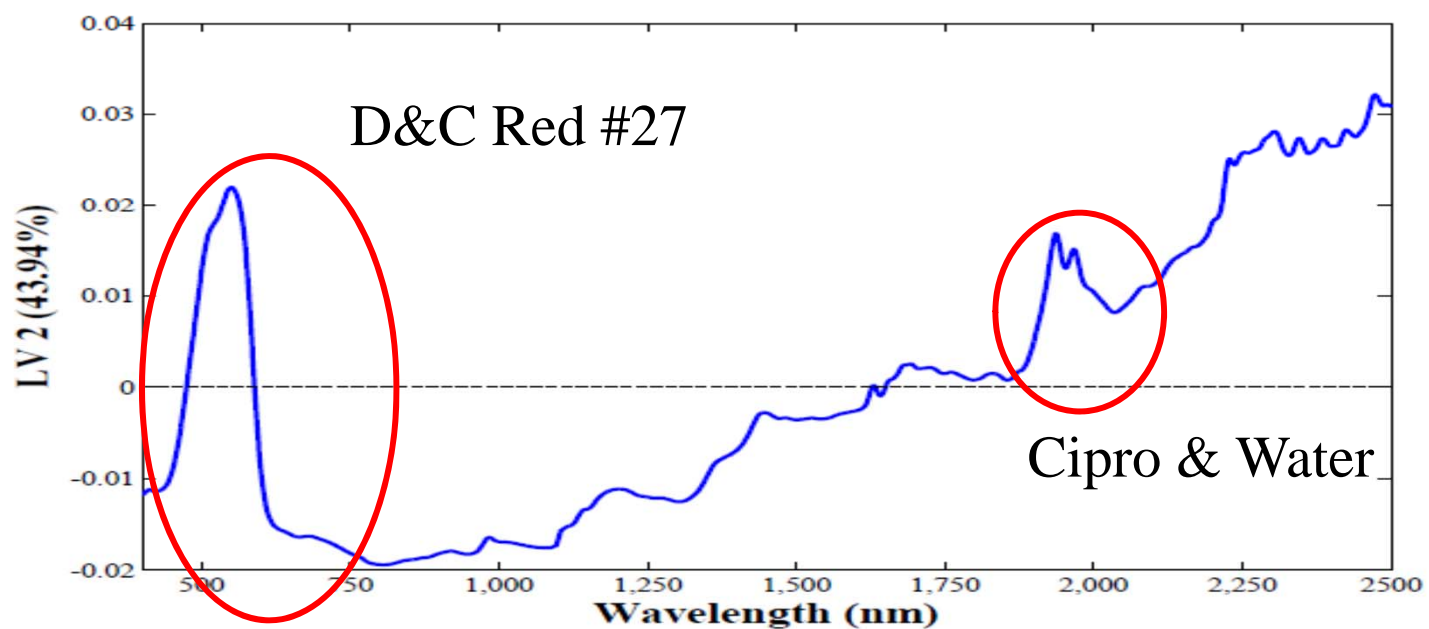
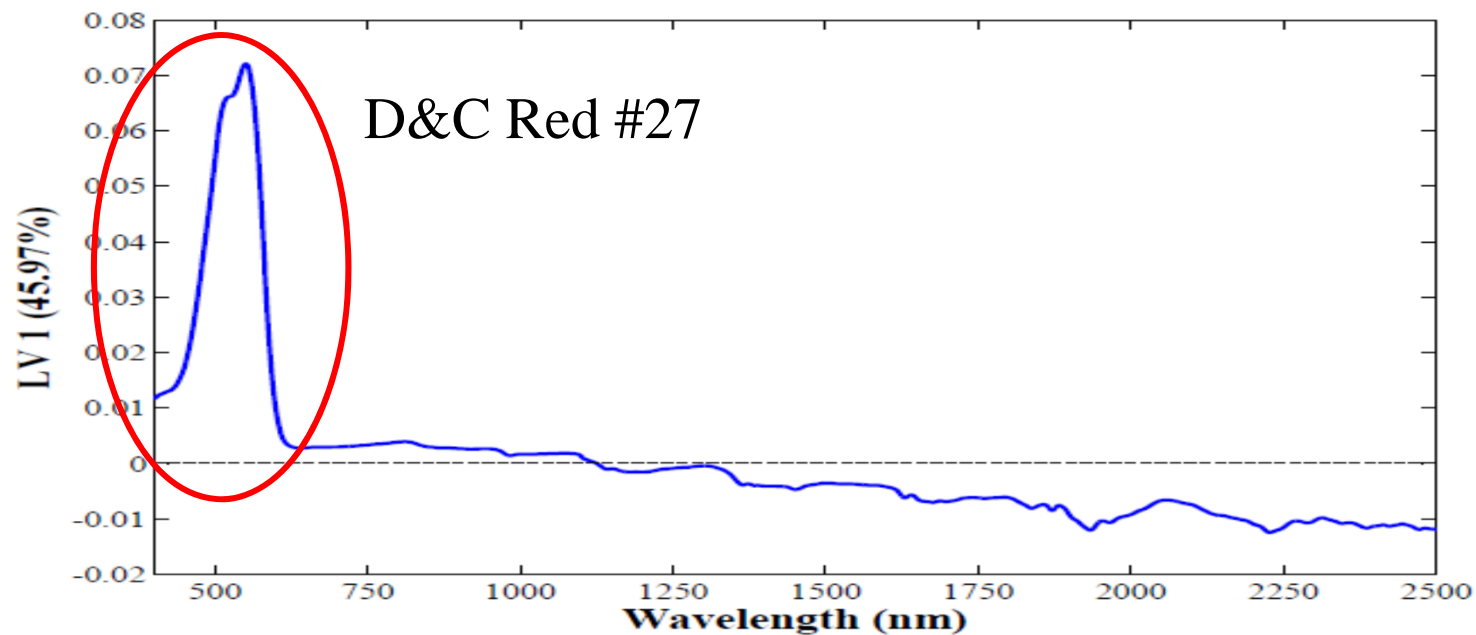


Calibration Model using RSM Batches

Legend – (Air volume-Product Temp-Curing Temp)



Loadings of the Latent Variables

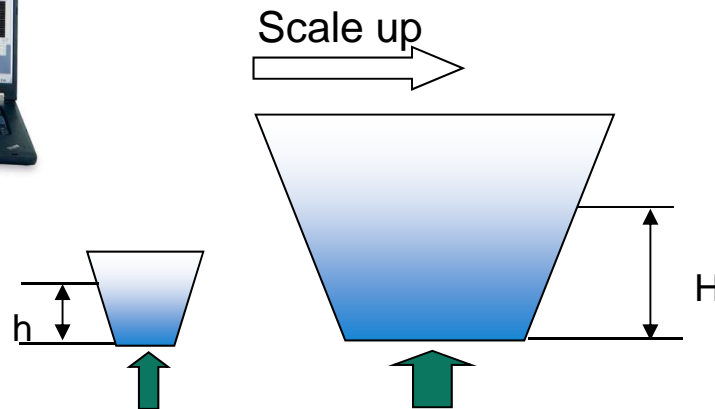


Scale Up Work Using Linear Approach

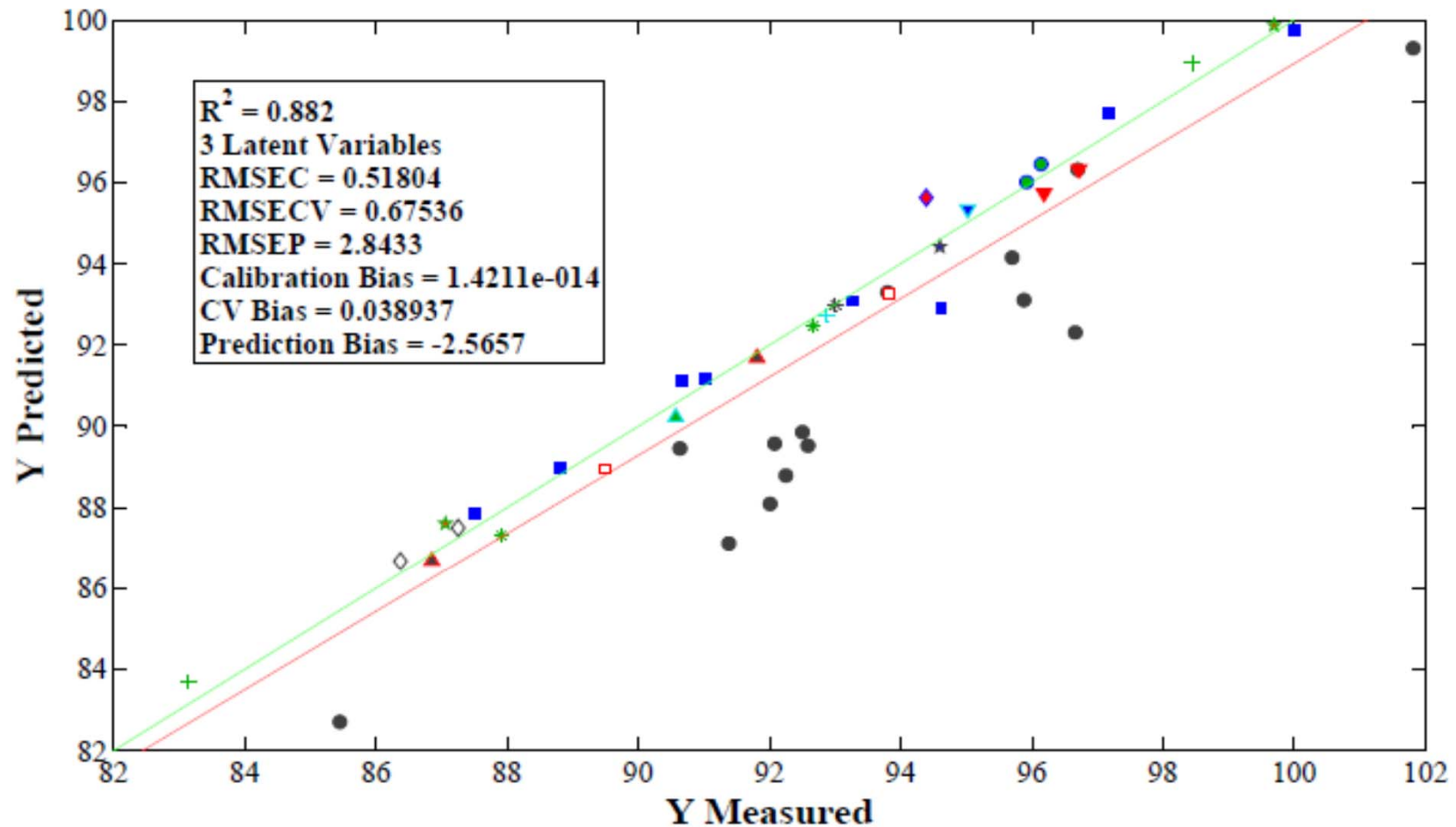
Non Critical Parameters Kept Constant = Microclimate and Atomization Pressure
Critical Process Parameters Based on Design Space = Product Temp. & Curing Temp.

Spray Rate (amount of solution sprayed/kg of material)
 $= S_1 * M_1 / S_2 * M_2$

Air Volume (air volume to bed size ratio)
 $= A_1 * M_1 / A_2 * M_2$



External Validation of the Predictive Model using Scale-Up Batches (Unilab Batches)



PE Summary

Process efficiency is key quality attribute that needs to be monitored

It depends upon:

Prod. Temp, Air volume, RH

95 – 100% Design space sweet spot

90 – 100% mostly good, but if low RH & combination of other parameters can get failures

Some model adjustments are needed when changing scale

Lower scale data is very useful

Model Details for PE

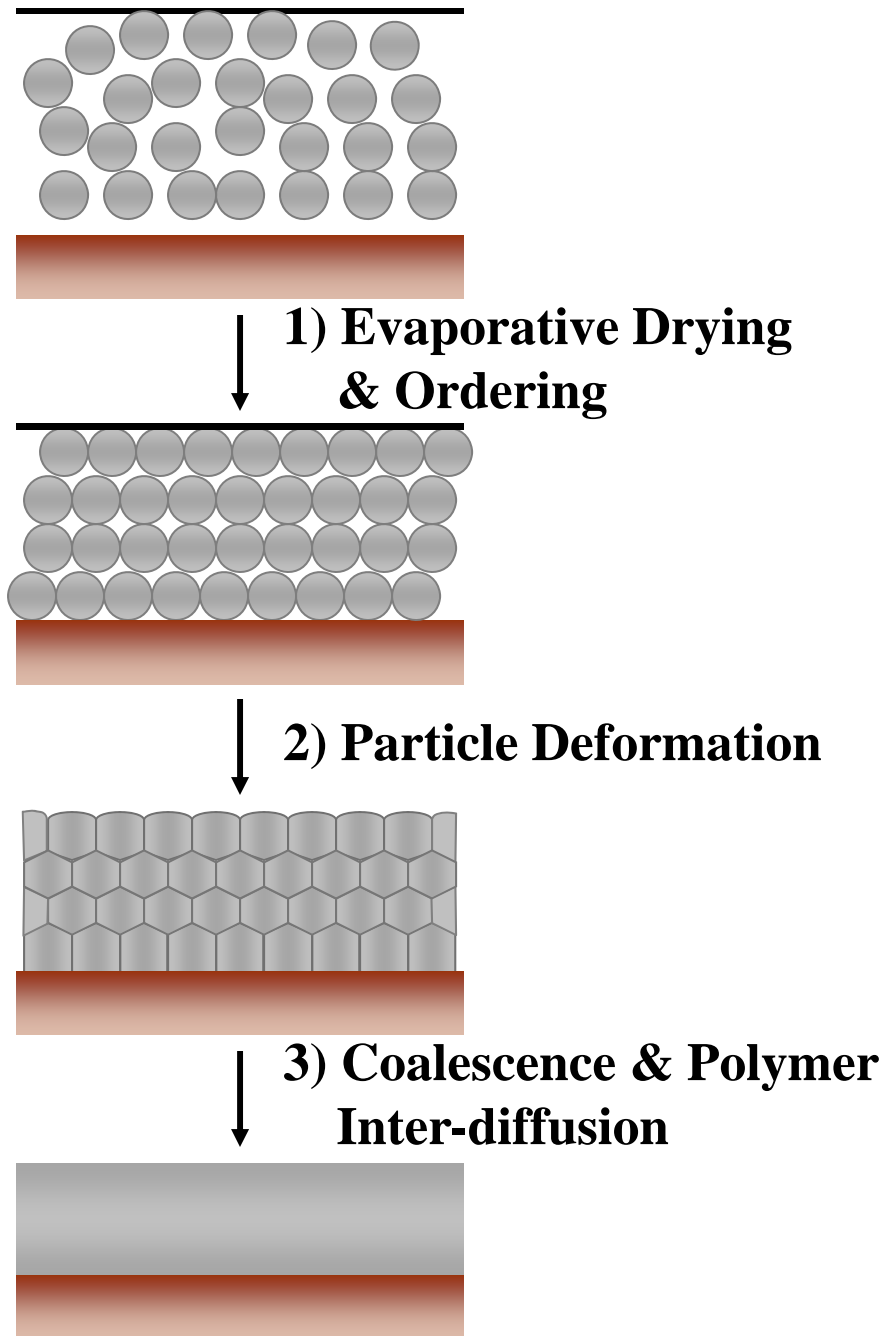
- Major change (variance) in Spectra Modeled
- D&C Red #27 Color Wavelength (557 nm) for determining polymer deposition i.e. Surrogate marker for process efficiency
- Wavelength range used for Modeling
 - 400-2500 nm with resolution of 0.5 nm
- Preprocessing of the X-block
 - Normalize (1-Norm, Area = 1), Smoothing (order: 0, window: 15 pt, incl only), Mean Center
- Preprocessing of the Y-block
 - Mean Center
- Latent Variables - 3
- Cross validation: venetian blinds with 5 splits
- No of Samples Utilized for Calibration Model – 30 uncured samples with varying process efficiency - RSM study



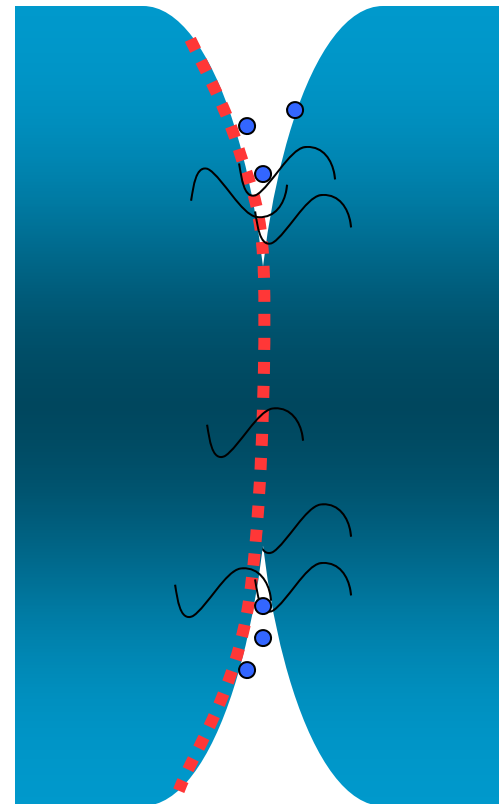
Outline

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Latex Particle Interface



Rate is very Temp.
Dependent
Coat @ $T \sim T_g$

Not to scale

Ethylcellulose Aqueous Dispersion

USP DEFINITION

“Ethylcellulose Aqueous Dispersion is a colloidal dispersion of Ethylcellulose in water. It contains NLT 90.0% and NMT 110.0% of the labeled amount of ethylcellulose. It contains suitable amounts of **Cetyl Alcohol** and **Na Lauryl Sulfate**, which assist in the formation and stabilization of the dispersion. It may contain suitable antifoaming and antimicrobial agents.”

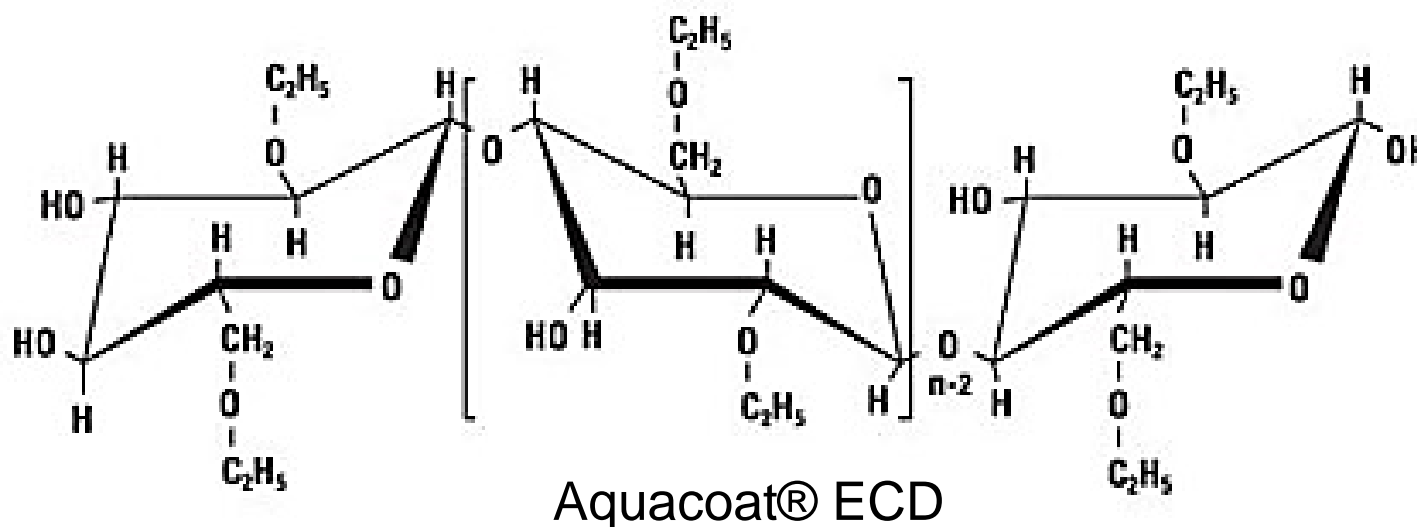
Ethylcellulose Tg 131-150°C

Aquacoat 30% dispersion (Tg = 91°C)

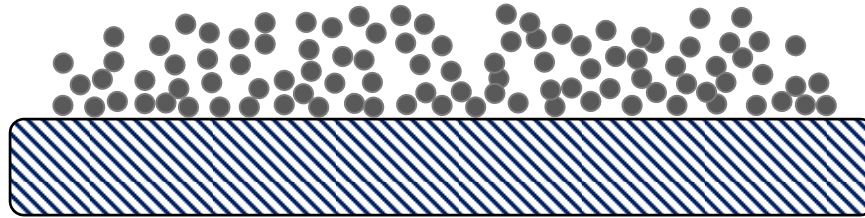
Aquacoat 30% dispersion + 25% w/w/ TEC = Tg 36-38°C

Aquacoat 30% dispersion particle size 85% < 500 nm

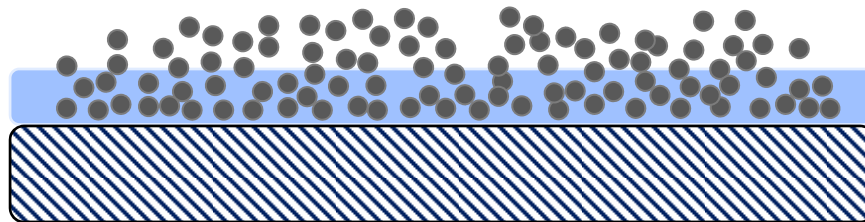
Water is critical to Tg



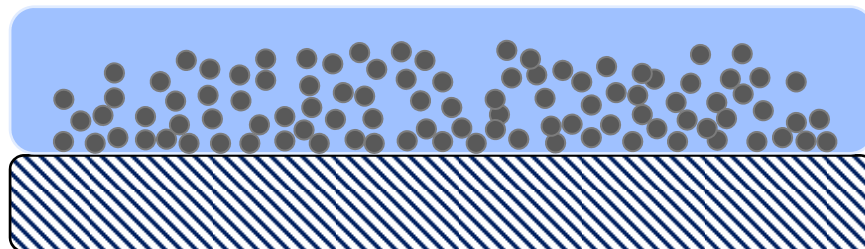
Film Formation and Water



Dry Sintering



Capillary Deformation



Wet Sintering

Interfacial Tension

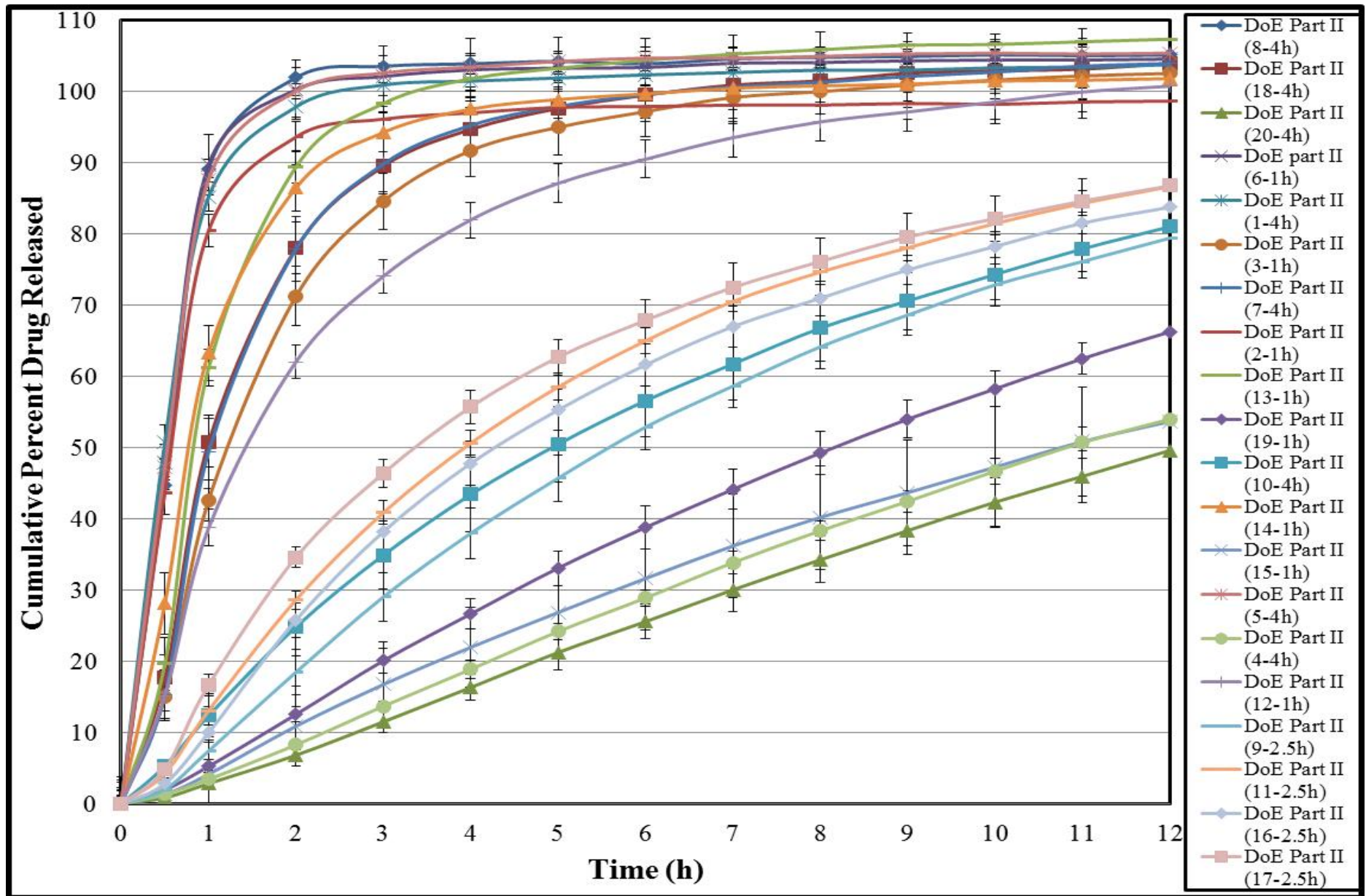
Particle / air

Water / air

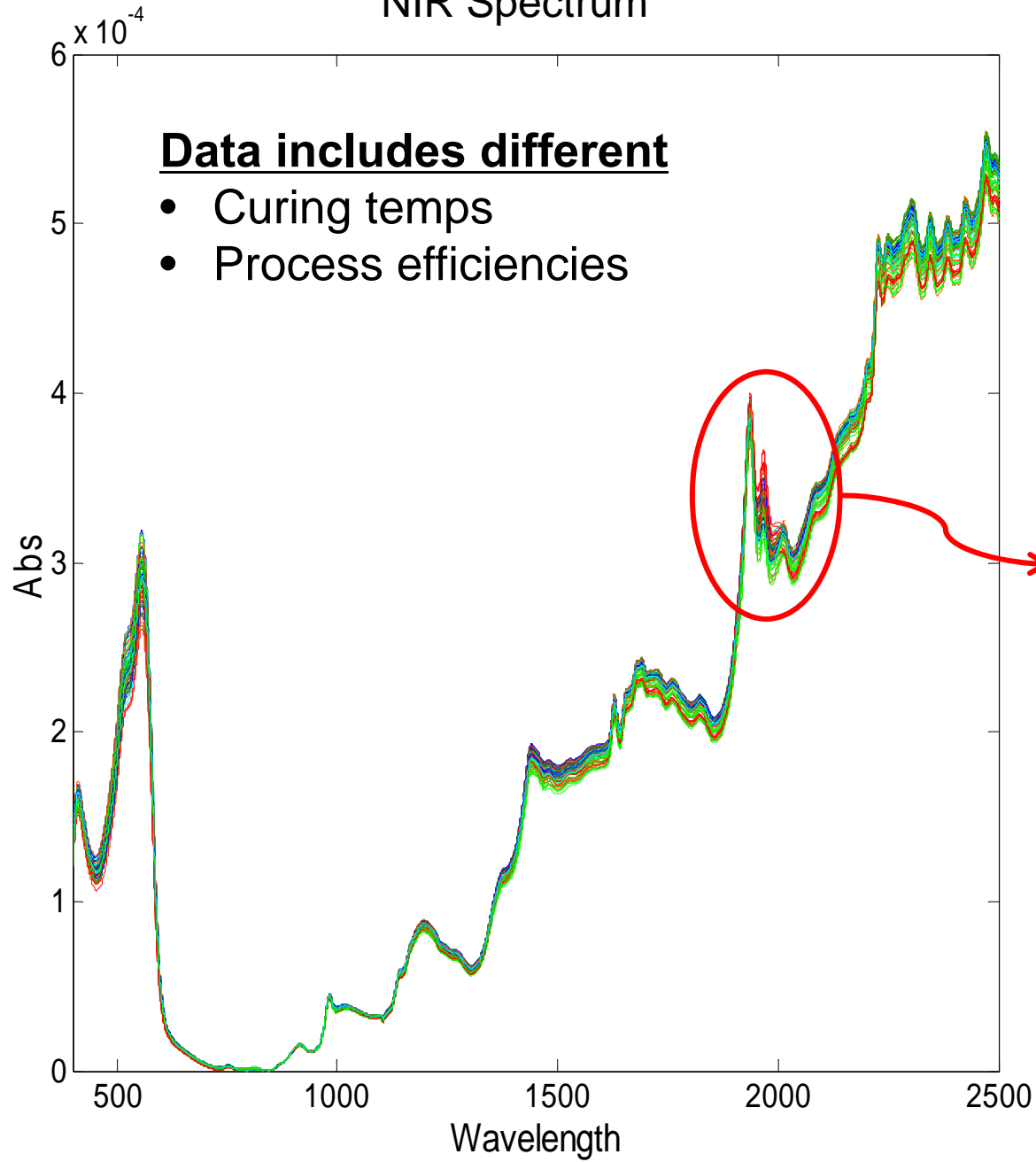
Particle / air

Particle / water

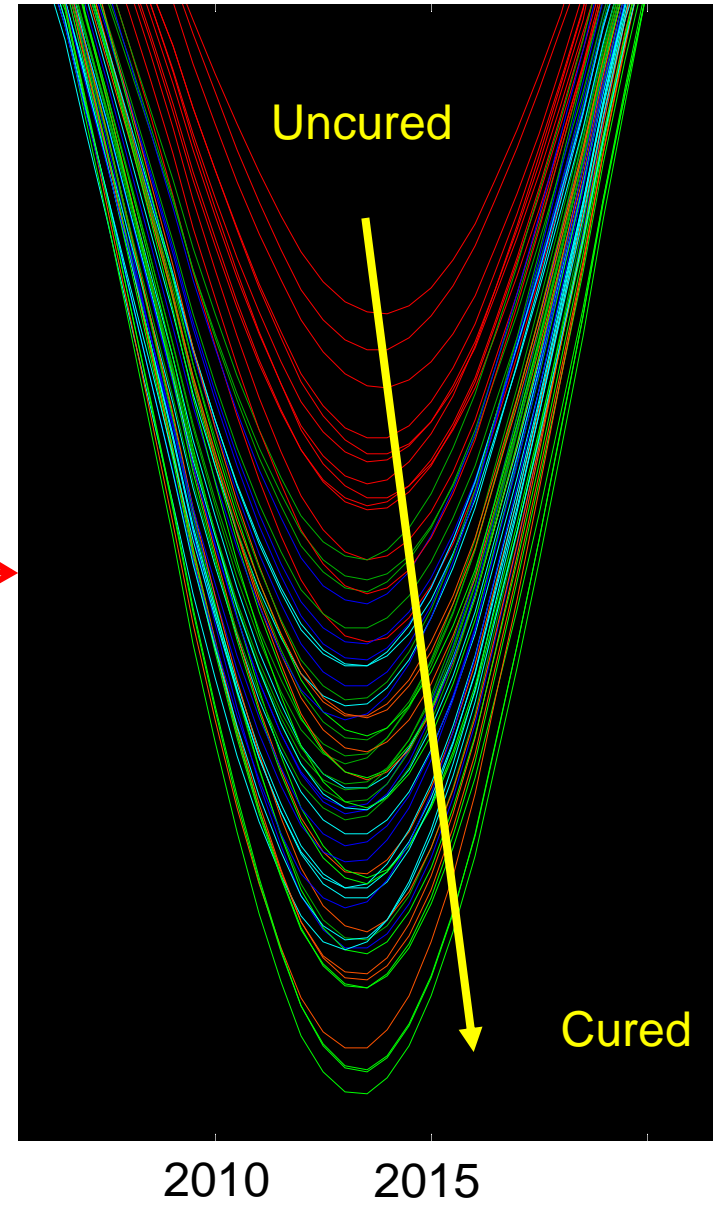
Dissolution Profiles of Ciprofloxacin HCl Bead Batches, 252 mg/g DoE – Part II (with center points)



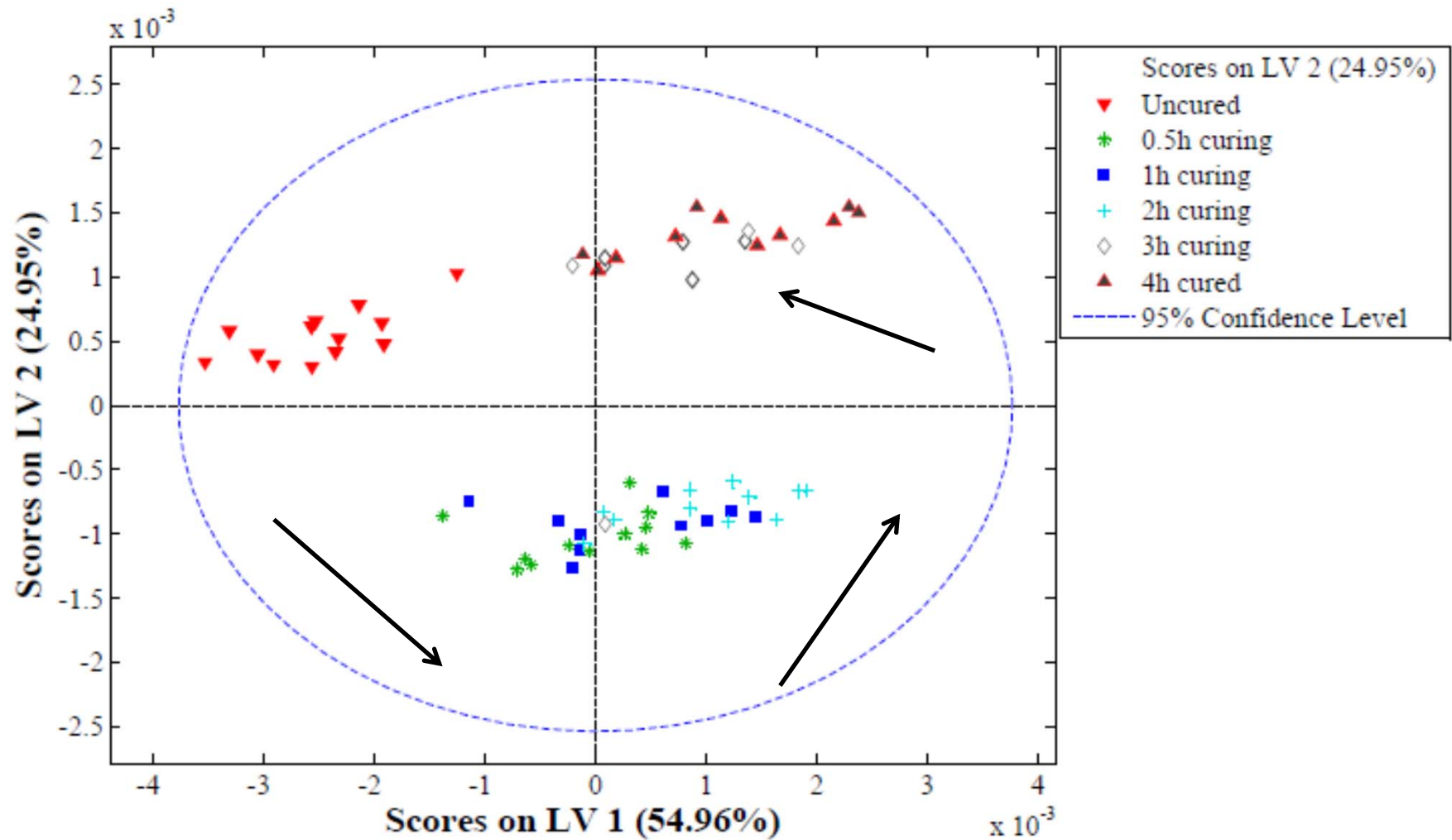
NIR Spectrum



2nd Derivative

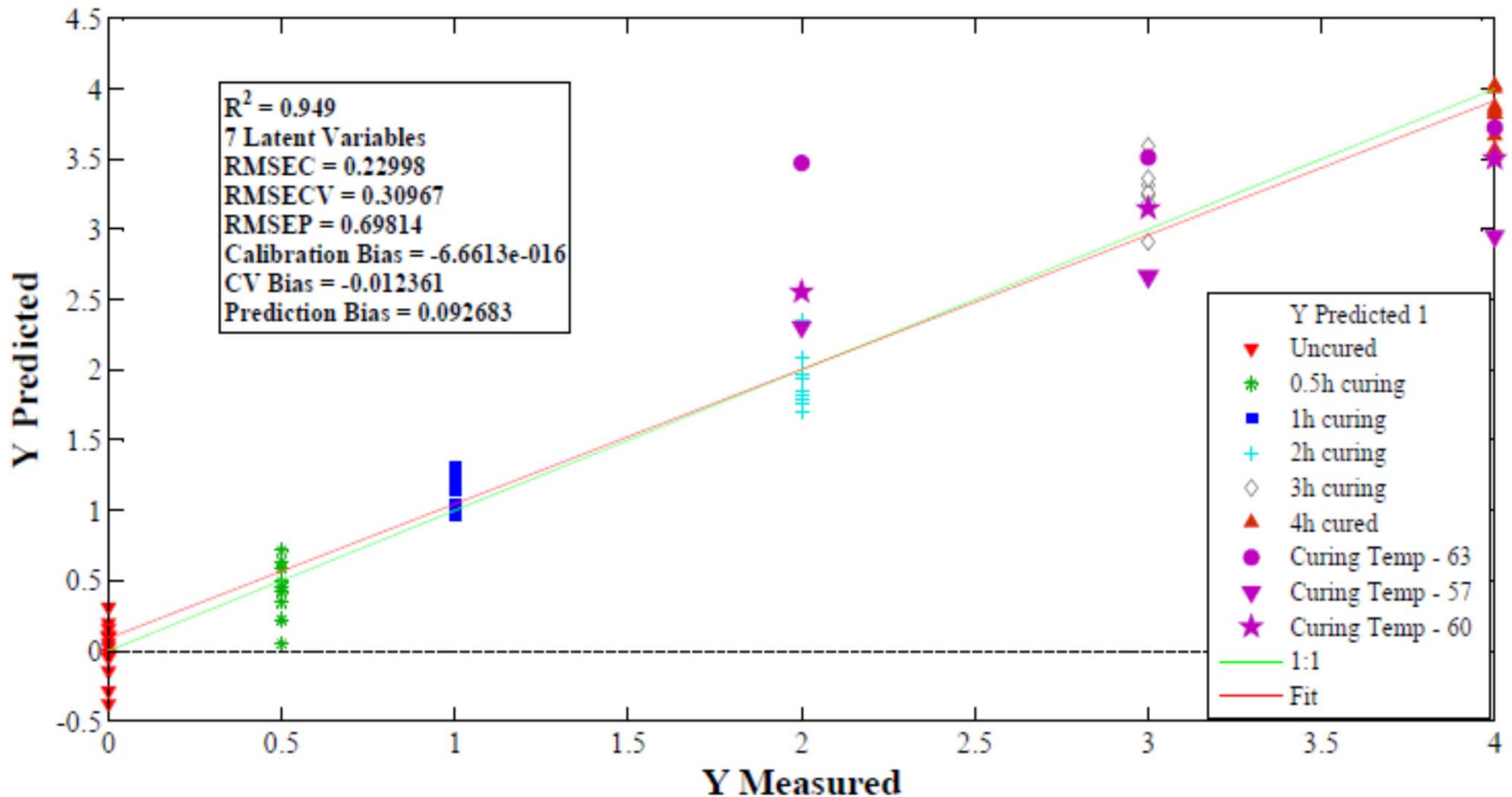


Scores Plot and Curing Process Trajectory



External Validation of the Predictive Model

Scale-Up Batches (Unilab) @ Different Curing Temperature



Low Curing Temperature batch will take longer time to reach optimum curing
Optimal Curing Temperature batch will take target time to reach optimum curing
Higher Curing Temperature will take less time to reach optimum curing

Model Details for Extent of Curing

Major change (variance) in Spectra Modeled

- Water Band and Ethylcellulose Band (~1950 nm) for change in surface moisture/residual moisture from the core of the beads

Wavelength range used for Modeling

- 400-2500 nm

Preprocessing of the X-block

- 2nd Derivative (order: 2, window: 15 pt, incl only), Smoothing (order: 0, window: 15 pt, incl only), Normalize, Mean Center

Preprocessing of the Y-block

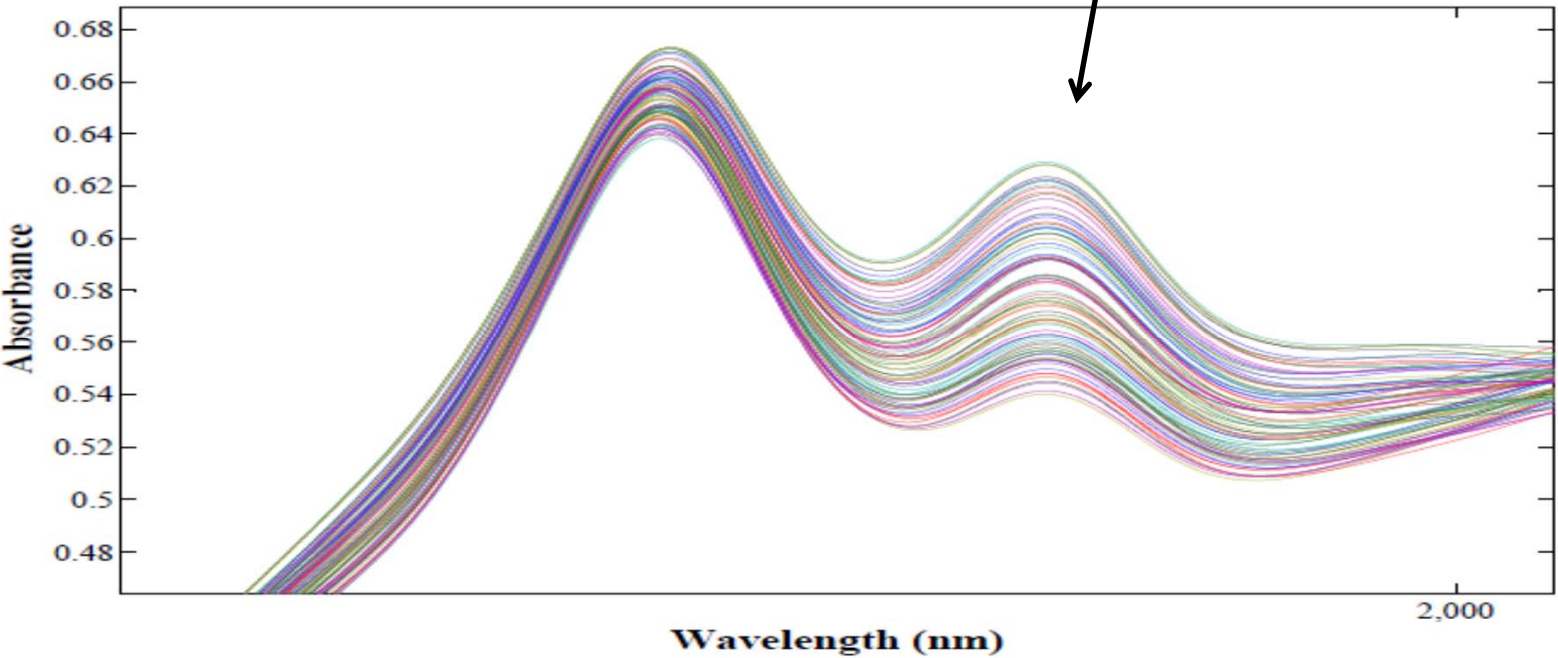
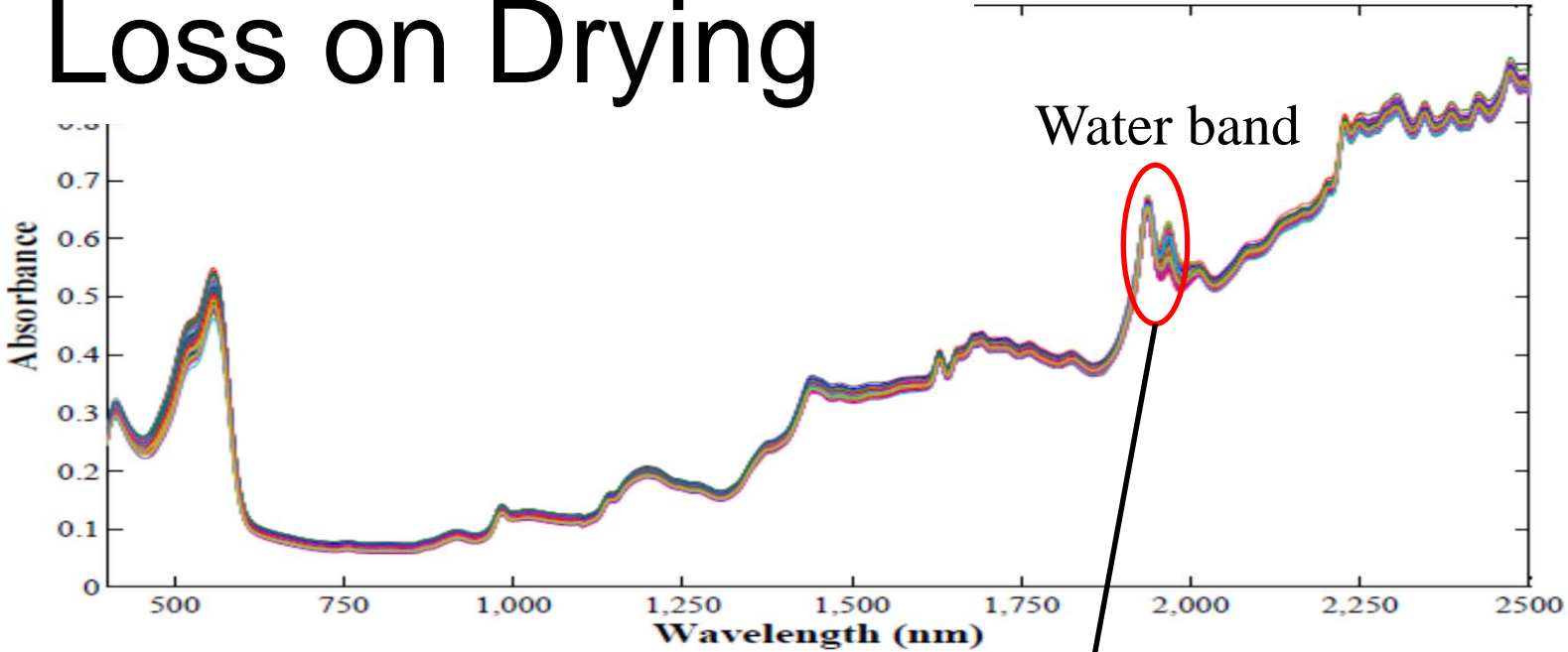
- Auto-scale

Latent Variables - 7

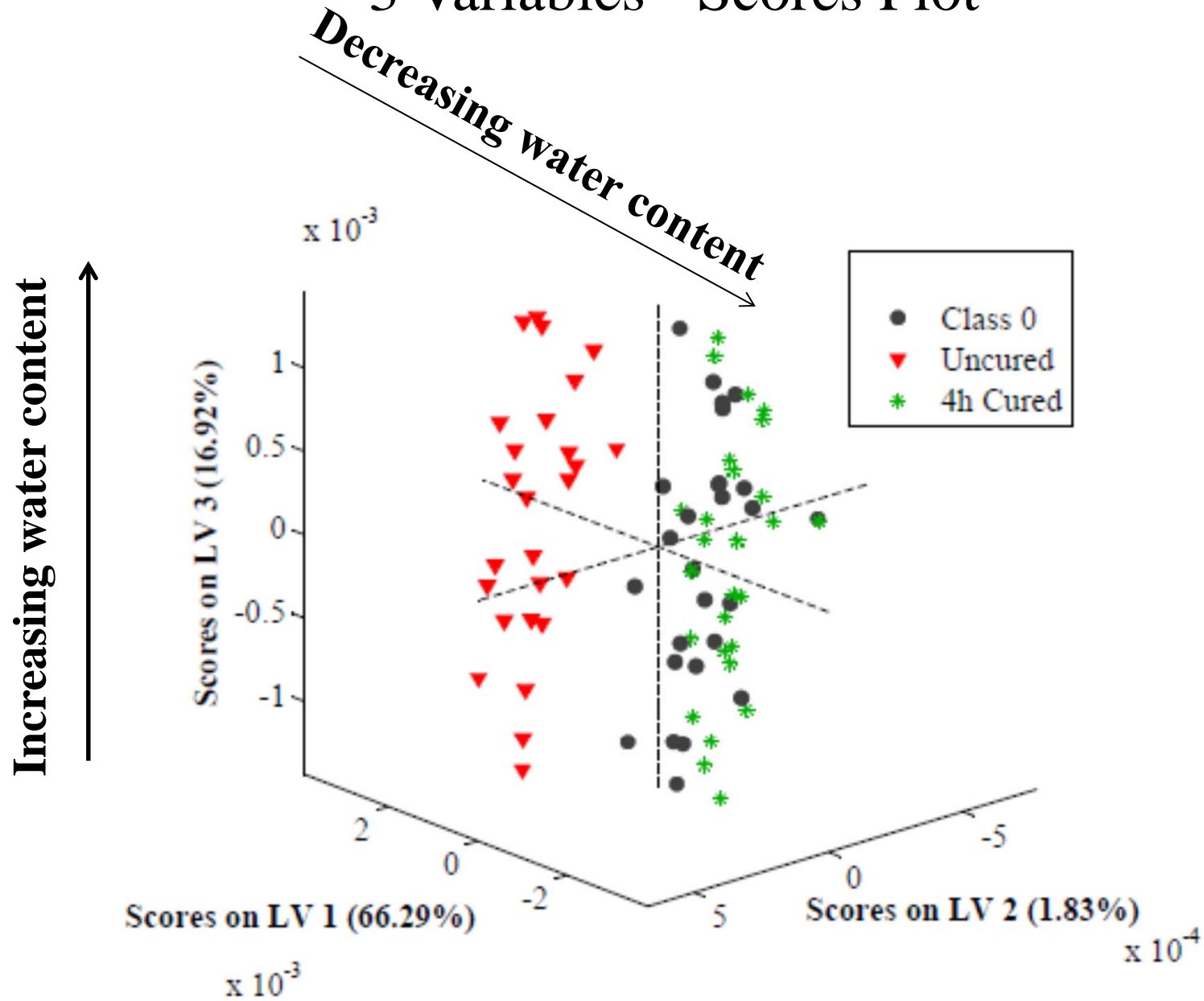
Cross validation: venetian blinds with 8 splits

No of samples used for calibration model – 66 samples (uncured, 0.5h, 1h, 2h, 3h and 4h cured beads)

Loss on Drying

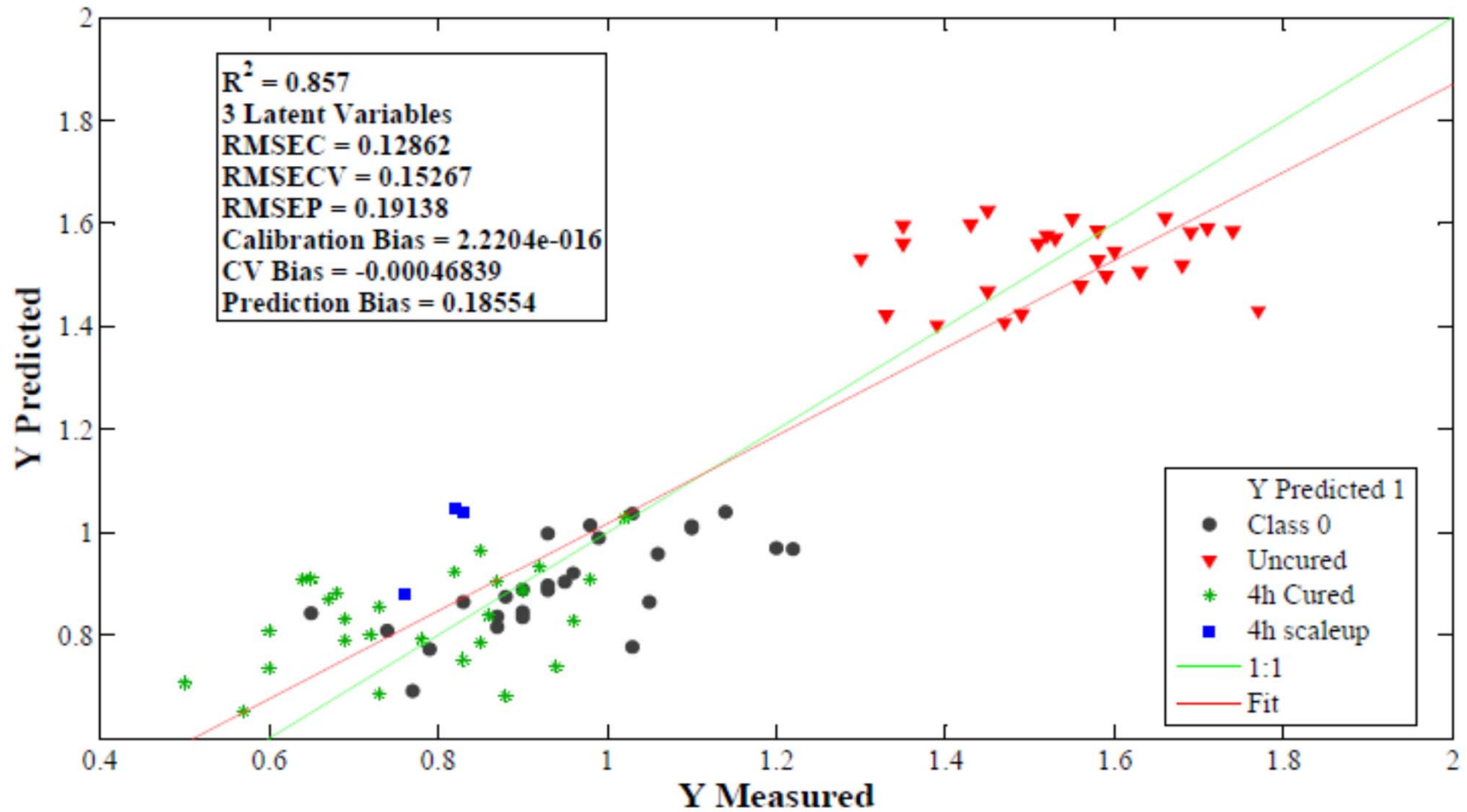


3 Variables - Scores Plot



External Validation of the Predictive Model

Scale-Up Batches (Unilab Batches)



Model Details for Loss on Drying

Major change (variance) in Spectra Modeled

Water Band (~1940 nm)

Wavelength range used for Modeling

400-2500 nm

Preprocessing of the X-block

1st Derivative (order: 2, window: 15 pt, incl only), Normalize (1- Norm, Area =1), Mean Center

Preprocessing of the Y-block

Auto-scale

Latent Variables - 3

Cross validation: venetian blinds w/ 9 splits

No of samples used for calibration model – 80 samples (RSM batches: Uncured, Design Point and 4h Cured)



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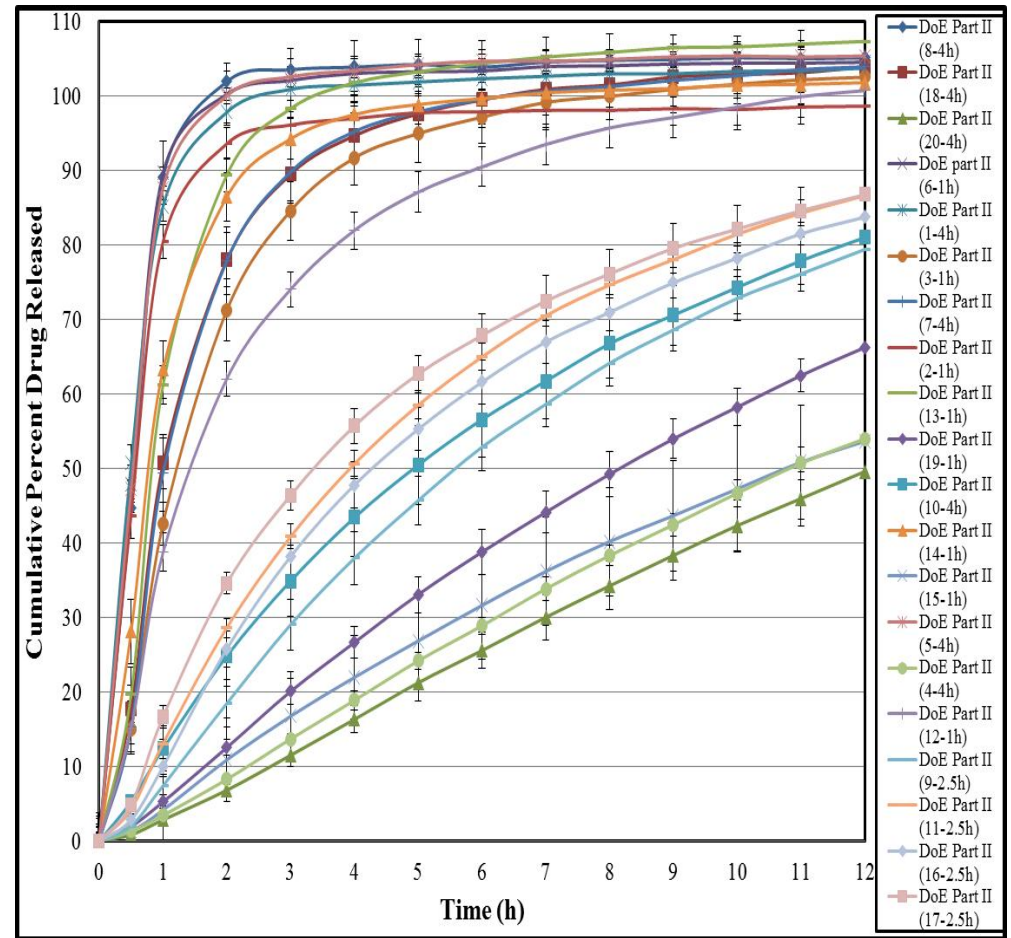
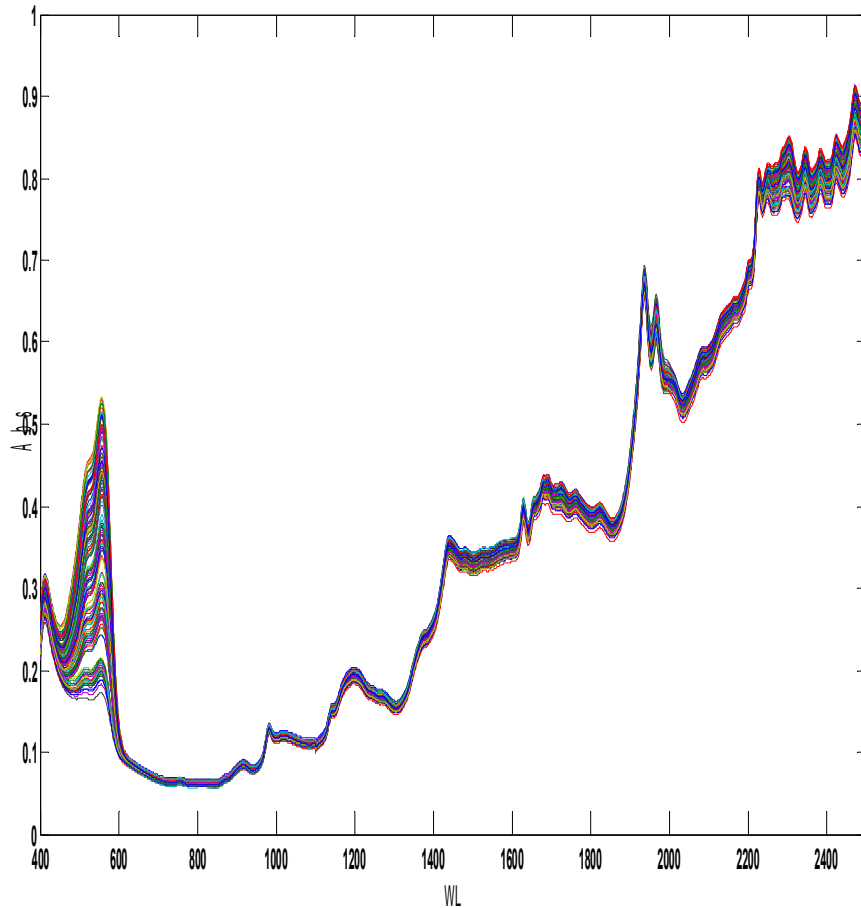
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 - **Dissolution & data fusion**
- Summary

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Dissolution Prediction: The Problem

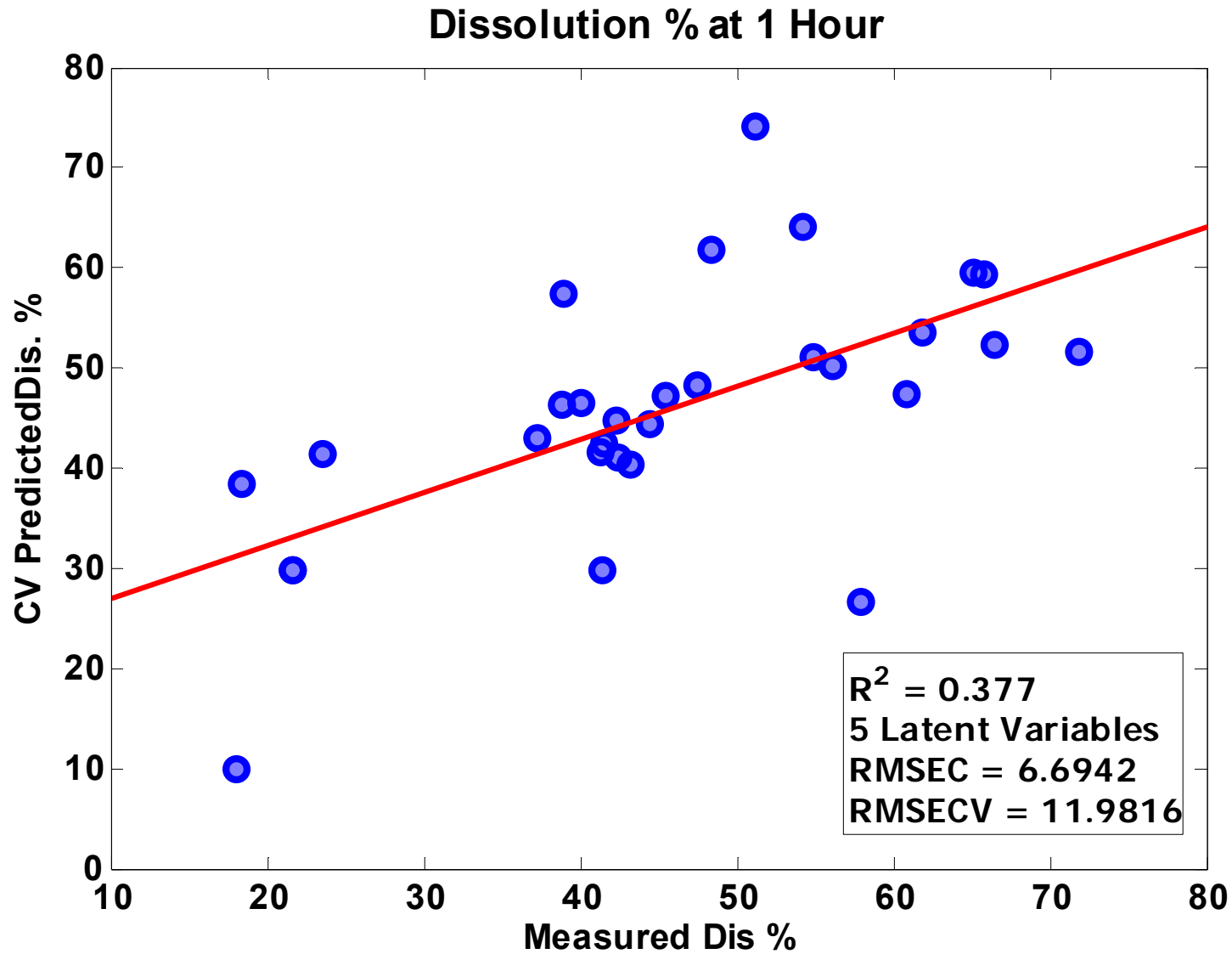
- Coating of Multiparticulate beads involves:
 - Spraying with a coating solution
 - Curing at higher temperature.
- Complex process involving optimization of many parameters :
 - **Process Parameters:** Product temperature, atomization air volume, curing temperature, curing time
 - **Environmental measurements:** Humidity
- Changes in any of these parameters can have an impact on the final product quality.

Dissolution Profiles

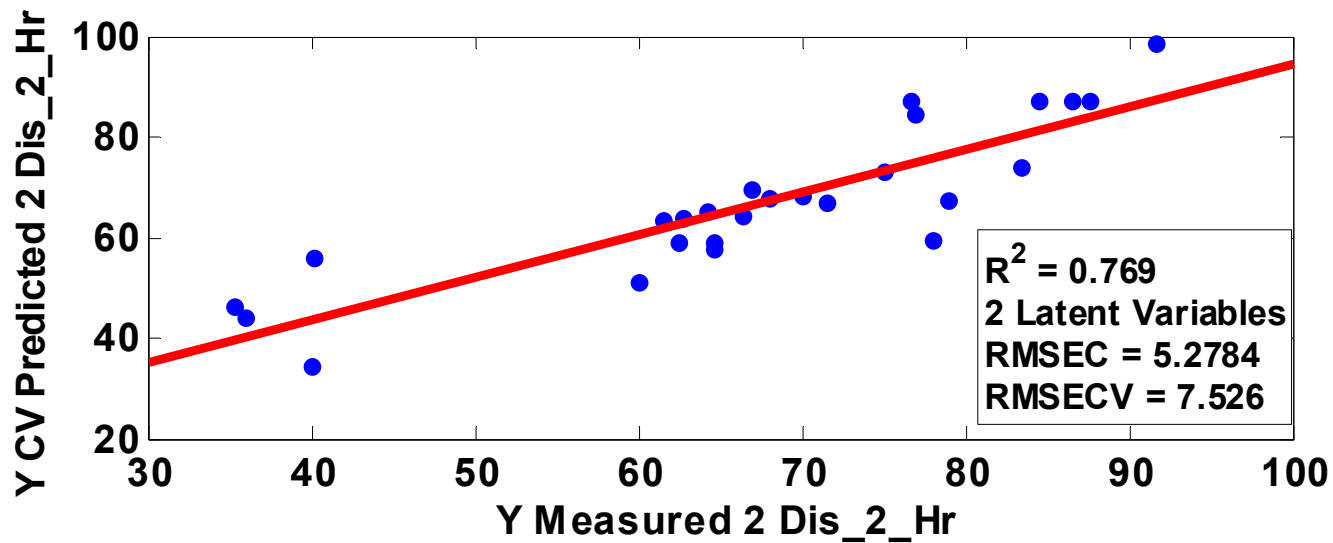
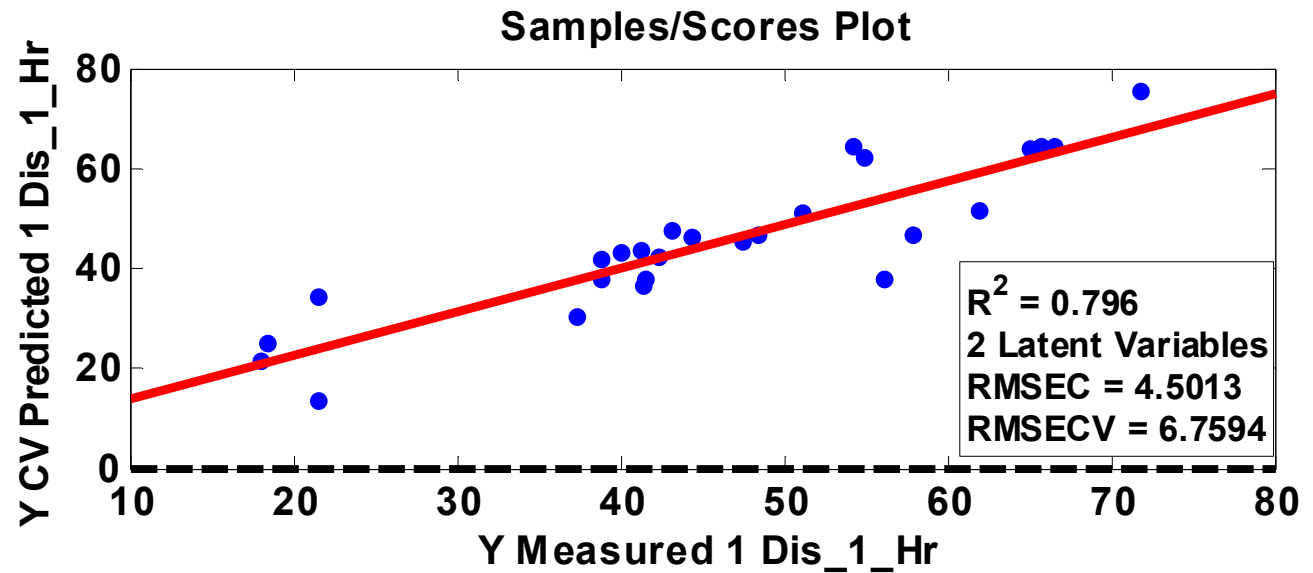


- Dissolution data is difficult to predict:
 - Physical property – typically weaker NIR signal
 - Depends upon many parameters

Prediction Using NIR Spectra Only

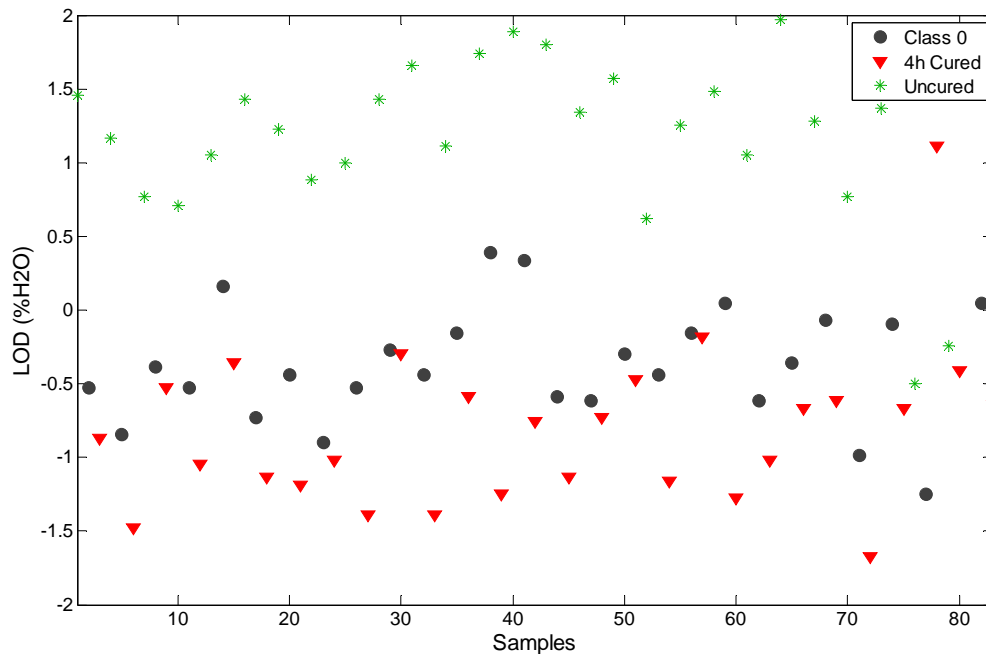


Prediction Using Process Data Only



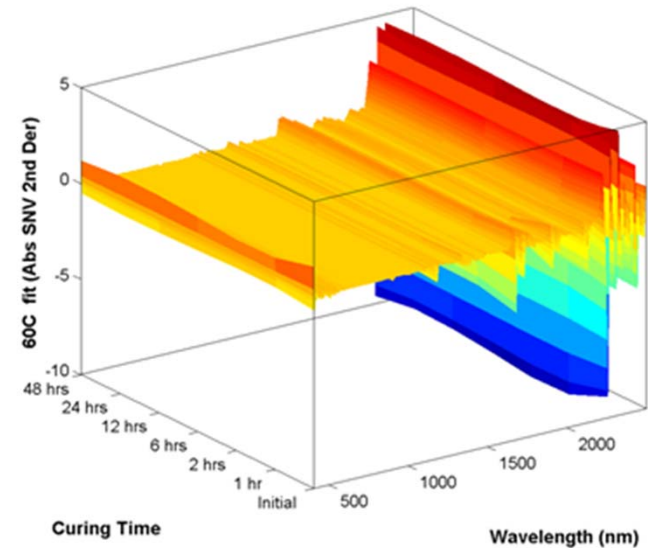
Data Fusion

- Environmental and spectral datasets very different structure
 - Spectral data will overwhelm environmental data
 - To fuse data need to reduce dimensions of spectral



1 Temp + RH every 15 sec
4 hr run = 1,920 data pts.

Environmental Data

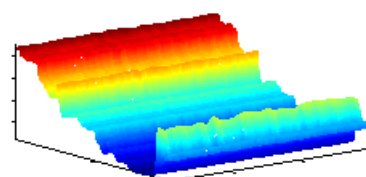
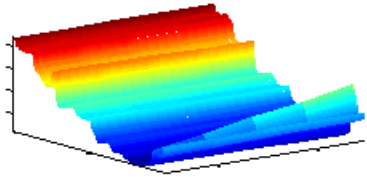


1 spectra every 2 min
4 hr run = 482,400 data pts.

Spectral Data

NIR of Spraying Process

NIR of Curing Process



Parafa
PCA

Parafc
PAC

Process
Param.

Spraying
Scores

Curing
Scores

Spraying Process

Curing Process

Air
Volume

Product
Temp.

Curing
Temp.

Curing
Time

Relative
Humidity

| Data Fusion | | | | | | |
|-----------------|-----------------|------------|--------------|-------------|-------------------|--|
| Spraying Scores | Spraying Scores | Air Volume | Curing Temp. | Curing Time | Relative Humidity | |

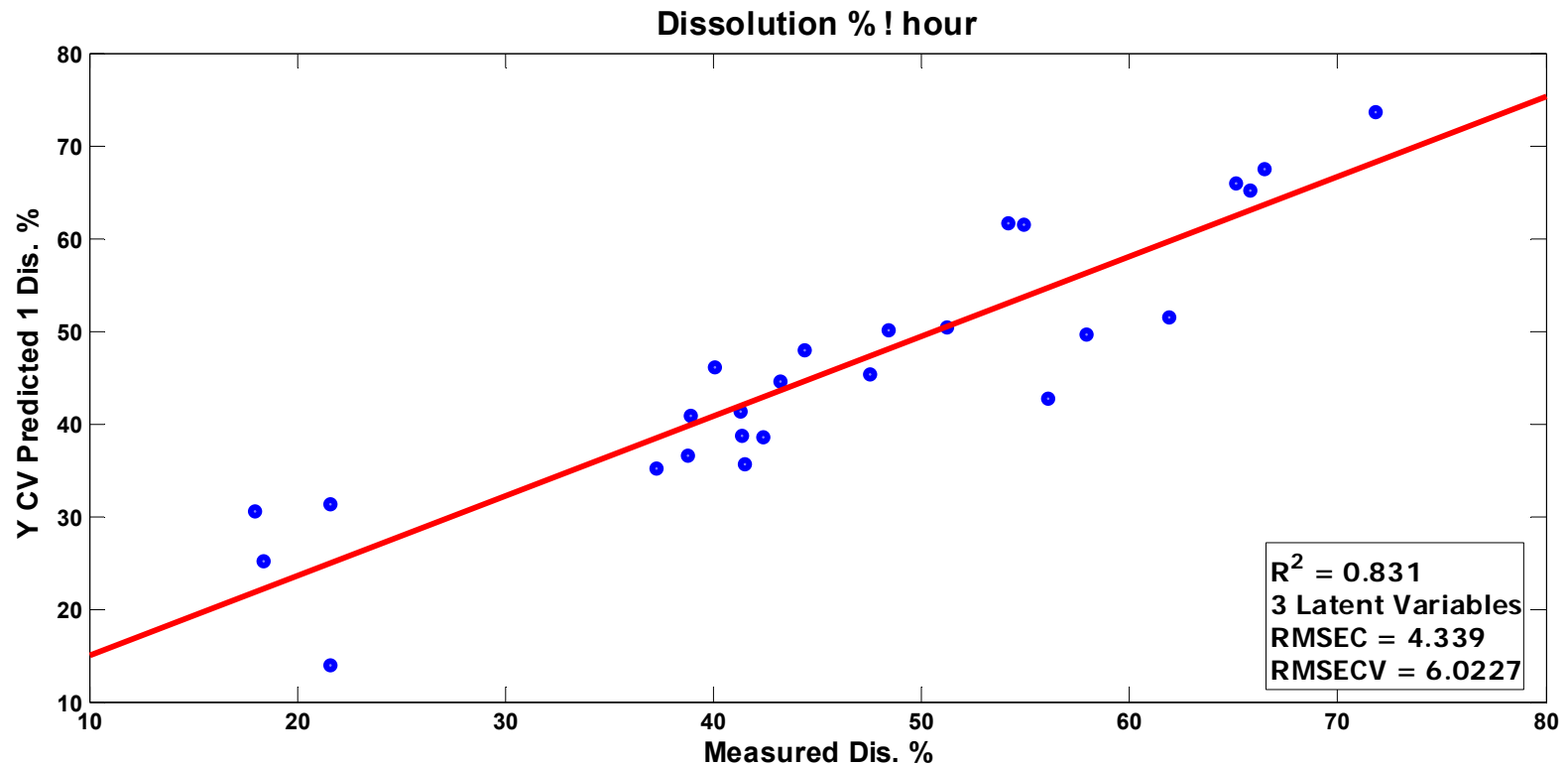
Dissolution
Results

PLS Model For Dissolution

Parafac = Parallel Factor Analysis

Dissolution 1Hour

Parafac Decomposition

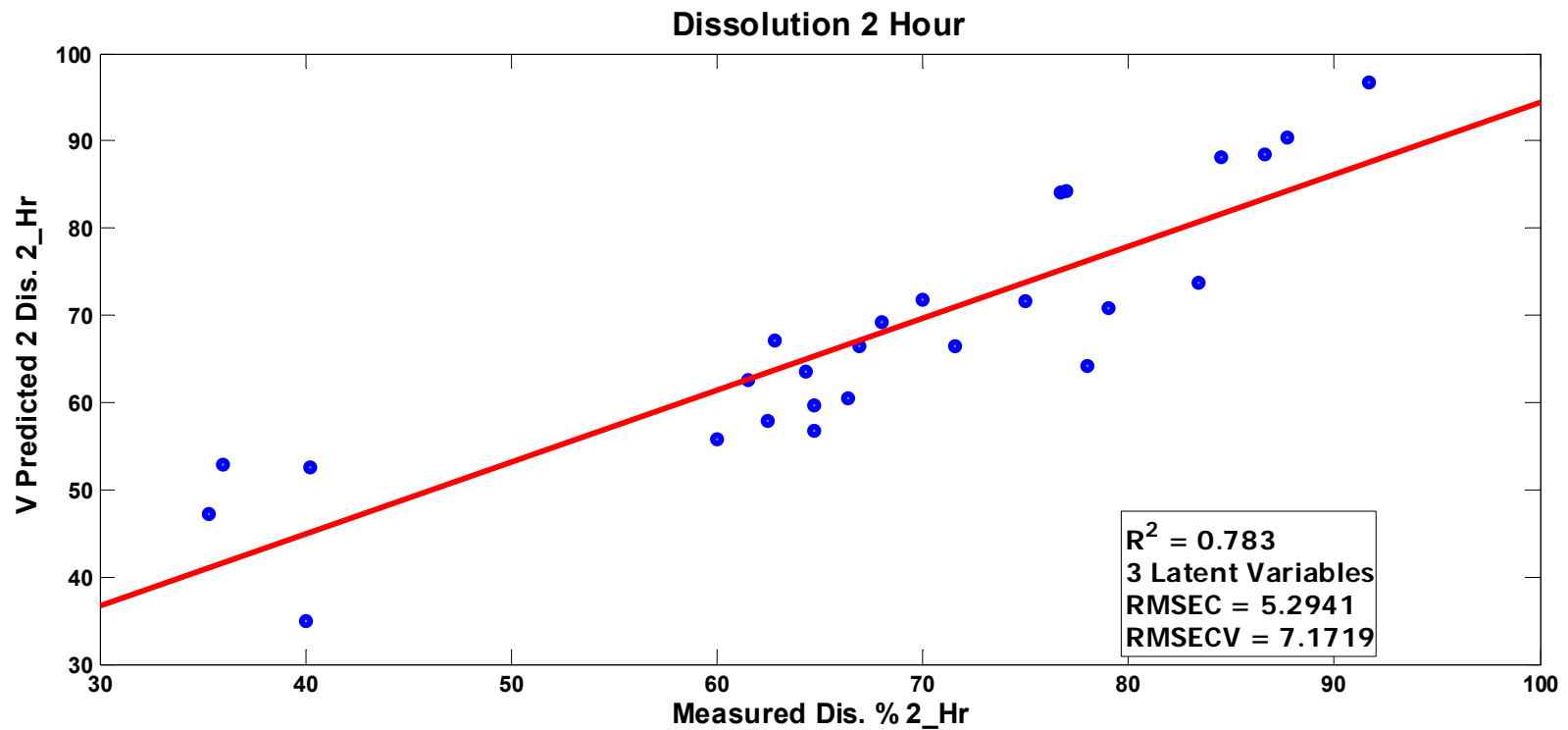


Parafac is similar to 3D multidimensional PCA and process time is the 3rd dimension

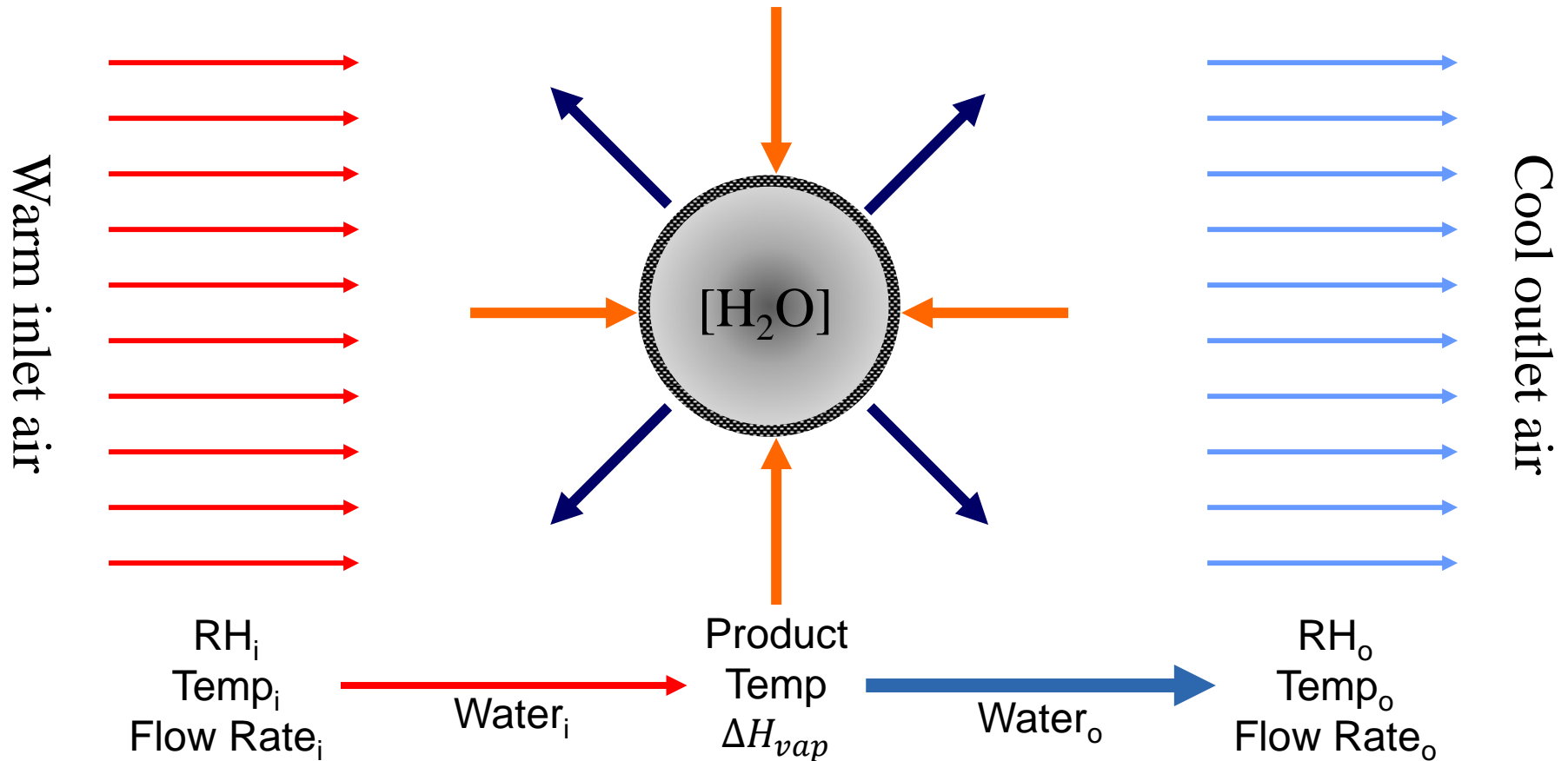
-Dimensions are: time, wavelength and batch No.

Dissolution 2 Hour

Parafac scores with Process data



Heat & Mass Transfer



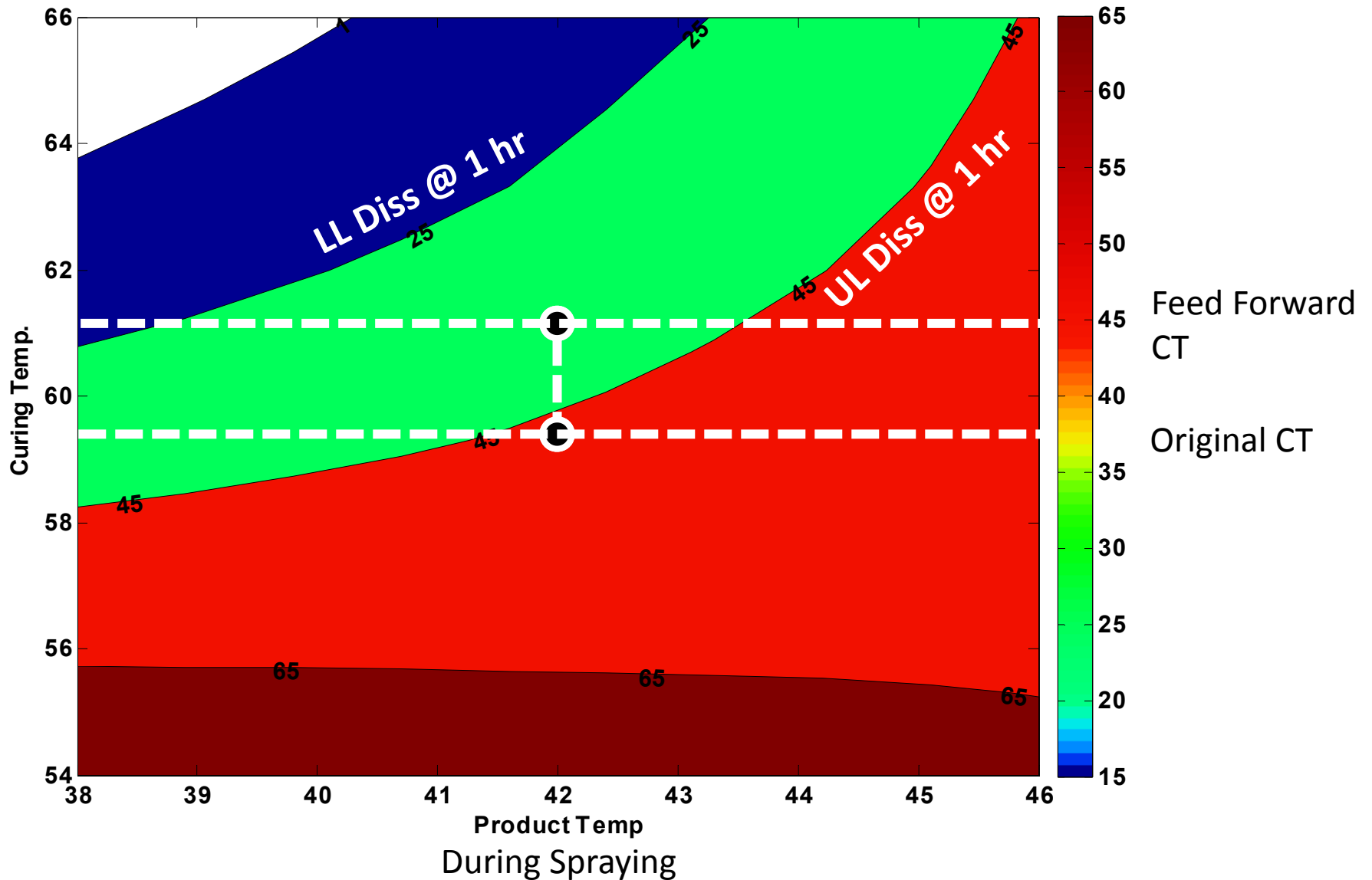
▤ Air liquid interface

→ Heat transfer (conduction, convection and radiation)

← Mass transfer (conduction and convection)

CT Feed-Forward for Diss. 1h

Simulation using PLS model



Control Strategy Summary

| Factor | Attribute | Range Studied | Target Range | Validated Range | Purpose of Control | Method of Control |
|---|---------------------------|--|---|--|---|----------------------------------|
| Drug Substance and Excipients - Critical Material Attribute | | | | | | |
| Ciprofloxacin HCl | Particle Size | d10 = _____, d50 = _____ d90 = _____ | Information unknown as the drug layered beads were procured directly from the vendor. | | To ensure batch to batch consistency | NIR –Laser (controlled Upstream) |
| Mannitol | Particle Size | d10 = _____, d50 = _____ d90 = _____ | | | | |
| Sugar Spheres | Particle Size | Fraction between 18 and 16 mesh | | | | |
| Povidone K-30 | K- value | Tight specs from the vendor | 29-32 | 29-32 | To ensure consistent binding property | Vendor Specs |
| Formulation Variables – Critical Material Attributes | | | | | | |
| Core type/Size | Type and PSD | Information unknown as the drug layered beads were procured directly from the vendor | | To ensure target assay and desired drug release | Theoretical - Design of Experiments (Full factorial $2^3 = 8 + 2$ center points = 10 experiments) | |
| Binder type | Type | | | | | |
| DS/Binder ratio | Concentration | | | | | |
| Drug Layering Process – Critical Process Parameters | | | | | | |
| Pan Coating | Product temperature | Information unknown as the drug layered beads were procured directly from the vendor | | To ensure target assay and desired drug release achieve consistently | Theoretical - Design of Experiments (Resolution V fractional factorial – two level design i.e. $2^{5-1} = 16 + 4$ center points = 20 experiments) | |
| | Atomization Pressure | | | | | |
| | Air volume | | | | | |
| | Flow rate of API/Mannitol | | | | | |
| | Spray rate of Binder | | | | | |
| Drug Layered Beads – Critical Quality Attributes (In-Process Controls) | | | | | | |
| Quality Attribute | Sample Type | | Specifications | | Control Strategy | |
| Assay | Composite Samples | | 95-105% of label claim | | NIR and HPLC | |
| Drug Release | Composite Samples | | Q80 % = 30 minutes | | Dissolution | |
| PSD | Composite Sample | | Retained on 14 and 16 mesh | | Laser Diffraction | |
| Moisture | Composite Sample | | NMT 2.0% | | LOD | |
| Surface Morphology | Composite Sample | | Smooth Surface | | Optical Microscopy | |

Control Strategy Summary

| Factor | Attribute | Range Studied | Target Range | Validated Range | Purpose of Control | Method of Control | |
|---|---|--|--------------|---|---|--|--|
| Coating Polymer and Excipients - Critical Material Attribute | | | | | | | |
| Drug Layered Beads | Assay Dissolution PSD Surface Morphology | Controlled – upstream | | | | | |
| Ethylcellulose dispersion | Ethoxy content Particle Size | Vendor Specifications | | | To ensure batch to batch consistency | Vendor – tight control | |
| Triethyl citrate | Viscosity | Vendor Specifications | | | | Vendor – tight control | |
| Formulation Variables – Critical Material Attributes | | | | | | | |
| Polymer lot | Content and PSD | Information not evaluated as the polymer type, plasticizer type its ratio are pre-determined based on project collaboration | | | To ensure target assay and desired drug release | Ideally, variables can be evaluated using Design of Experiments (Full factorial 2 ³ = 8 + 2 center points = 10 experiments) | |
| Plasticizer type | Type | | | | | | |
| Polymer/plasticizer ratio | Concentration | | | | | | |
| Coating Process – Critical Process Parameters | | | | | | | |
| Fluid Bed Coating | Microclimate | <p>Information still being collected, experiments conducted in different stages</p> <ol style="list-style-type: none"> Evaluation of CPP using Neat Polymer System (Resolution V Fractional factorial) Determination of Process range study (including batch size and coating level along with spray rate optimization (OFAT approach as interactions terms not interested) Screening of CPP using information from earlier stages (Resolution IV Fractional factorial in two blocks (with and without center points) Response surface methodology using identified CPP to determine optimum operating conditions and design space Confirmation of the design space using full factorial design on next scale equipment | | | | | |
| | Atomization Pressure | | | | | | |
| | Product temperature | | | | | | |
| | Air volume | | | | | | |
| | % Solids | | | | | | |
| | Curing Temperature | | | | | | |
| | Curing Time | | | | | | |
| | Humidity | | | | | | |
| Coated Beads – Critical Quality Attributes (In-Process Controls) | | | | | | | |
| Quality Attribute | | Sample Type | | Specifications | | Control Strategy | |
| Assay | | Composite Samples | | 95-105% of label claim | | NIR and HPLC | |
| Drug Release | | Composite Samples | | 1h, 2h, 4h and 7h until 80% drug released | | NIR and dissolution | |
| PSD | | Composite Sample | | Retained on 14 and 16 mesh | | Laser Diffraction | |
| Moisture | | Composite Sample | | NMT 2.0% | | LOD | |
| Surface Morphology | | Composite Sample | | Smooth Surface | | Optical Microscopy | |

Conclusions

- This study demonstrated the ability of NIR spectroscopy as real-time process monitoring and end point determination tool during the fluid bed spraying and coating
- NIR coupled with environmental monitoring could serve as a powerful process analytical technology tools to improve process understanding and establish control
- **Future research need:** to use NIR data to create feed back loop based upon actual product state
 - i.e., adaptive manufacturing
 - Key barrier getting instruments and models to talk to each other



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